

# *Modeling and Simulation in Porous Media*

*in Honor of Jean Roberts & Jérôme Jaffré*

*Rocquencourt, December 8-9 2014*

## *Total Differential interpolation of Two-phase Data for Three-phase Compressible Flows*

**Guy Chavent \***

**Raphaël DiChiara-Roupert\*\***

**Gerhard Schäfer\*\***

\* CEREMADE, Université Paris-Dauphine, and INRIA-Rocquencourt

\*\* LYGES, EOST Strasbourg

# Summary

- Three-phase compressible equations
- Choice of pressure unknown :  
    water, oil or gas versus global ?
- TD-condition  $\Leftrightarrow$  existence of a global capillary function  $P_{cg}$
- Interpolation of TD-three-phase data from two-phase data
- Numerical results
- Conclusions

# Three-phase Compressible equations

- Classical resolution (1=water, 2=oil, 3=gas) :  
solve for the **oil pressure**  $P_2$  the “pressure equation” :

$$\frac{\partial}{\partial t} \left\{ \phi \sum_{j=1}^3 B_j S_j \right\} + \nabla \cdot q = 0 ,$$

where  $q$  is the **global** volumetric flow vector:

$$q = \sum_{j=1}^3 \varphi_j = -Kd \left\{ \nabla P_2 + f_1 \nabla P_c^{12} + f_3 \nabla P_c^{32} - \rho g \nabla Z \right\}$$

$$\left\{ \begin{array}{l} d(s_1, s_3, p_2) = \sum_{j=1}^3 kr_j d_j = \text{global mobility,} \\ f_j(s_1, s_3, p_2) = kr_j d_j / \lambda = j^{\text{th}} \text{ fractional flow, } \sum_{j=1}^3 f_j = 1, \\ \rho(s_1, s_3, p_2) = \sum_{j=1}^3 f_j \rho_j = \text{global density.} \end{array} \right.$$

# Three-phase Compressible equations

- Classical resolution (1=water, 2=oil, 3=gas) :  
solve for the **oil pressure**  $P_2$  the “pressure equation” :

$$\frac{\partial}{\partial t} \left\{ \phi \sum_{j=1}^3 B_j S_j \right\} + \nabla \cdot q = 0 ,$$

where  $q$  is the **global** volumetric flow vector:

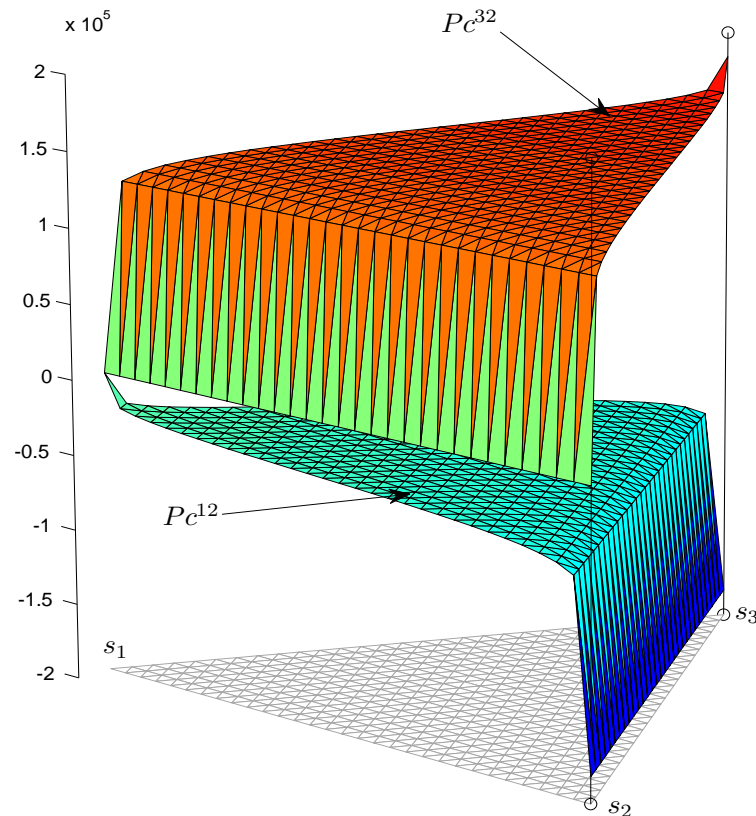
$$q = \sum_{j=1}^3 \varphi_j = -Kd \left\{ \nabla P_2 + f_1 \nabla P_c^{12} + f_3 \nabla P_c^{32} - \rho g \nabla Z \right\}$$

$$\left\{ \begin{array}{l} d(s_1, s_3, p_2) = \sum_{j=1}^3 kr_j d_j = \text{global mobility,} \\ f_j(s_1, s_3, p_2) = kr_j d_j / \lambda = j^{\text{th}} \text{ fractional flow, } \sum_{j=1}^3 f_j = 1, \\ \rho(s_1, s_3, p_2) = \sum_{j=1}^3 f_j \rho_j = \text{global density.} \end{array} \right.$$

Is **oil pressure** a better unknown than **water** or **gas pressure** ?

# Pressure unknown: water, oil or gas? (1)

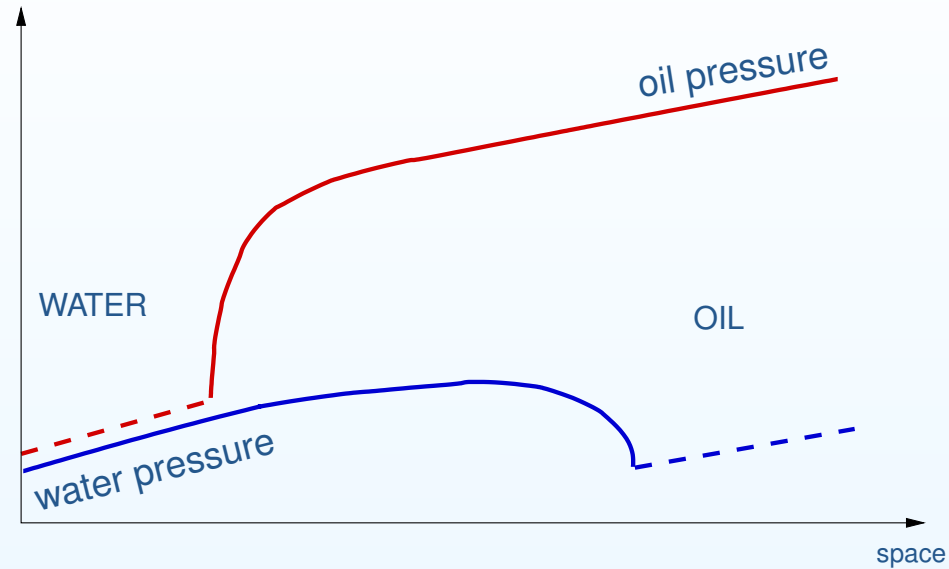
- Capillary pressures (Van Genuchten):  
they depend only on the **wetting phase** saturation !



top:  $P_c^{32} = P_{gas} - P_{oil}$

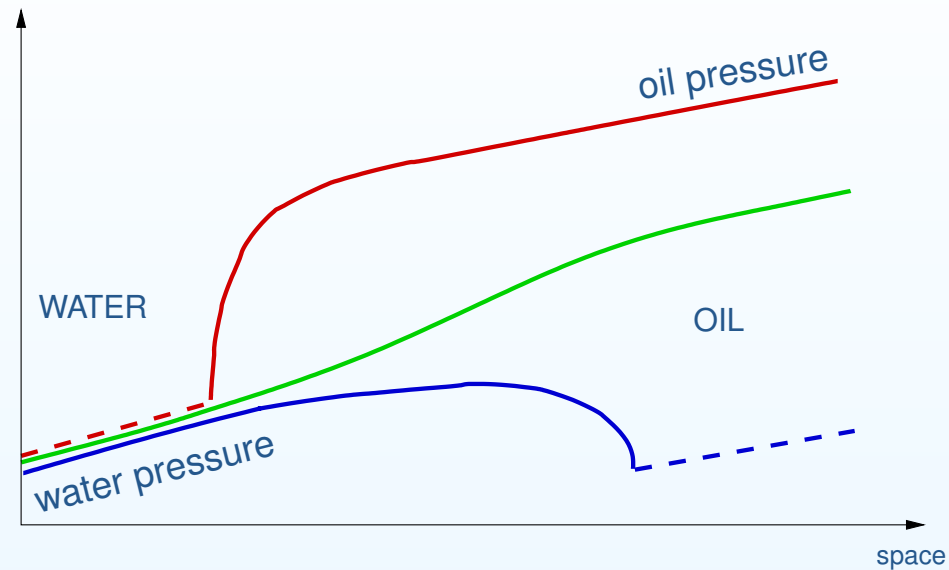
bottom :  $P_c^{12} = P_{water} - P_{oil}$

# Let us have a dream...



- **Does there exists** a pressure field  $(x, t) \rightsquigarrow P$  such that :

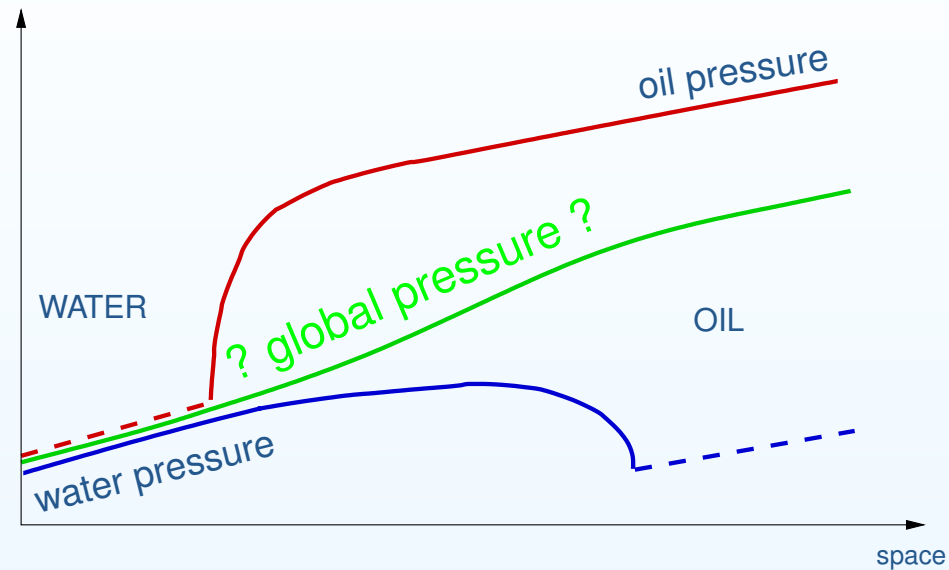
# Let us have a dream...



- Does there exist a pressure field  $(x, t) \rightsquigarrow P$  such that :

$P$  is smooth ,  $P_{water} \leq P \leq P_{oil}$

# Let us have a dream...



- Does there exist a pressure field  $(x, t) \rightsquigarrow P$  such that :

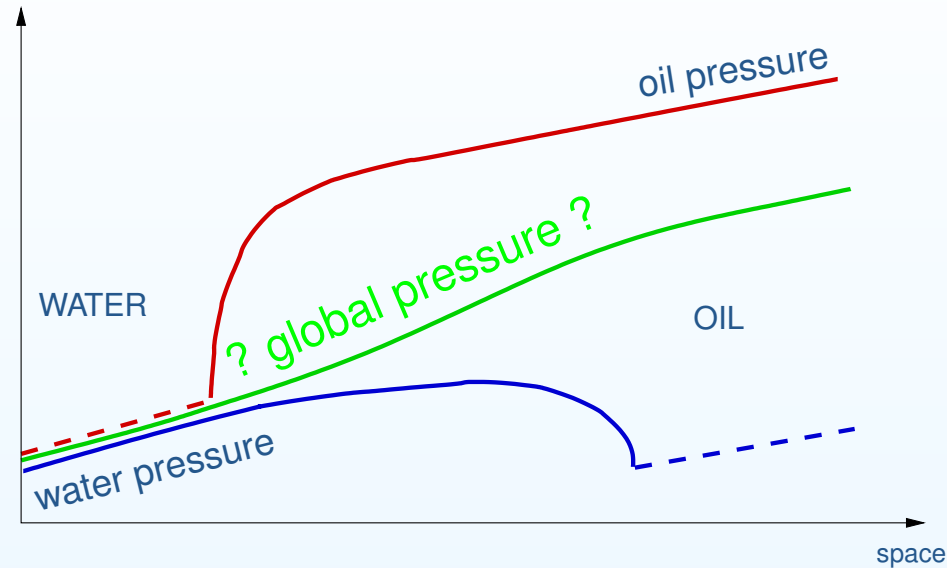
$$P \text{ is smooth} \quad , \quad P_{water} \leq P \leq P_{oil}$$

and  $P$  governs the global volumetric flow vector  $q$  :

$$q = -Kd(s_1, s_3, P) \{ \quad \nabla P - \rho g \nabla Z \} \quad ?$$



# Let us have a dream...



- Does there exist a pressure field  $(x, t) \rightsquigarrow P$  such that :

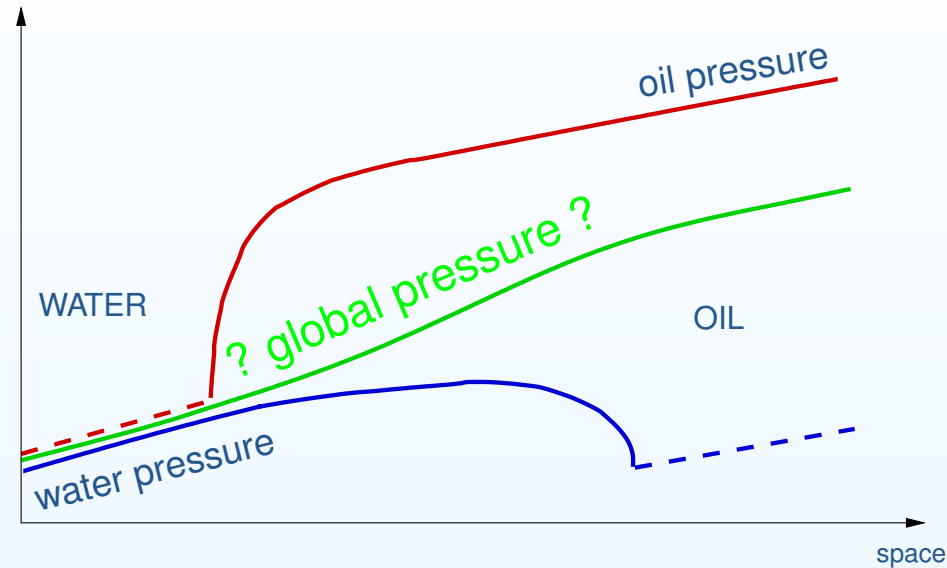
$$P \text{ is smooth} \quad , \quad P_{water} \leq P \leq P_{oil}$$

and  $P$  governs the global volumetric flow vector  $q$  :

$$q = -Kd(s_1, s_3, p) \left\{ (1 - \partial P_{cg} / \partial P) \nabla P - \rho g \nabla Z \right\} \quad ?$$

- 2-phase flow: **YES** (CJ 1986, AJ 2008),

# Let us have a dream...



- Does there exist a pressure field  $(x, t) \rightsquigarrow P$  such that :

$$P \text{ is smooth} \quad , \quad P_{water} \leq P \leq P_{oil}$$

and  $P$  governs the global volumetric flow vector  $q$  :

$$q = -Kd(s_1, s_3, p) \left\{ (1 - \partial P_{cg} / \partial P) \nabla P - \rho g \nabla Z \right\} \quad ?$$

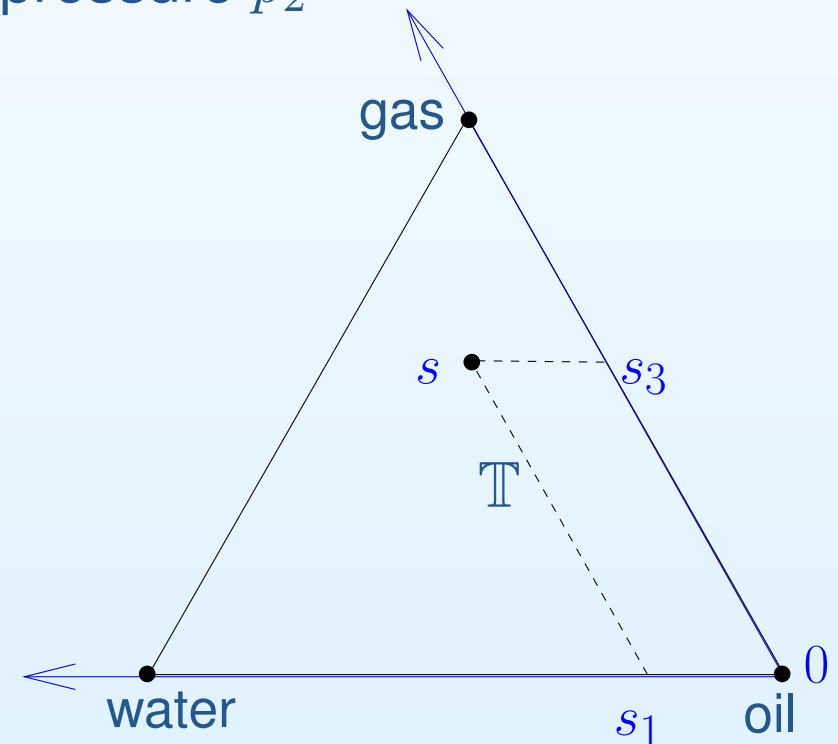
- 2-phase flow: **YES** (CJ 1986, AJ 2008), 3-phase flow: **YES IF ...**

## Total Differential Condition (GC, Applicable Analysis 2009)

- There exists a **Global Capillary Pressure function**  $P_{cg}$  s. t. :

$$\left\{ \begin{array}{l} \frac{\partial P_{cg}}{\partial S_1}(s_1, s_3, p) = f_1(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{12}}{dS_1}(s_1), \\ \frac{\partial P_{cg}}{\partial S_3}(s_1, s_3, p) = f_3(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{32}}{dS_3}(s_3), \end{array} \right.$$

for  $P_{\min} \leq p \leq P_{\max}$ ,  $s = (s_1, s_3) \in \mathbb{T}$ .



## Total Differential Condition (GC, Applicable Analysis 2009)

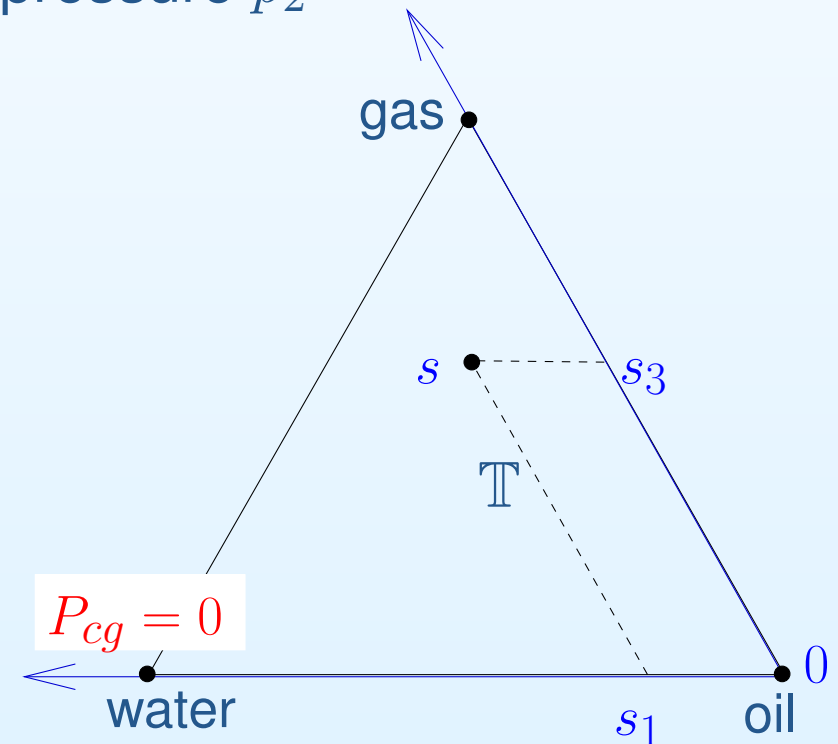
- There exists a **Global Capillary Pressure function**  $P_{cg}$  s. t. :

$$\left\{ \begin{array}{l} \frac{\partial P_{cg}}{\partial S_1}(s_1, s_3, p) = f_1(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{12}}{dS_1}(s_1), \\ \frac{\partial P_{cg}}{\partial S_3}(s_1, s_3, p) = f_3(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{32}}{dS_3}(s_3), \end{array} \right.$$

for  $P_{\min} \leq p \leq P_{\max}$ ,  $s = (s_1, s_3) \in \mathbb{T}$ .

- Condition  $p_1 \leq p \leq p_3$  is satisfied if :

$$P_{cg}(1, 0, p) = 0$$



## Total Differential Condition (GC, Applicable Analysis 2009)

- There exists a **Global Capillary Pressure function**  $P_{cg}$  s. t. :

$$\left\{ \begin{array}{l} \frac{\partial P_{cg}}{\partial S_1}(s_1, s_3, p) = f_1(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{12}}{dS_1}(s_1), \\ \frac{\partial P_{cg}}{\partial S_3}(s_1, s_3, p) = f_3(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{32}}{dS_3}(s_3), \end{array} \right.$$

for  $P_{\min} \leq p \leq P_{\max}$ ,  $s = (s_1, s_3) \in \mathbb{T}$ .

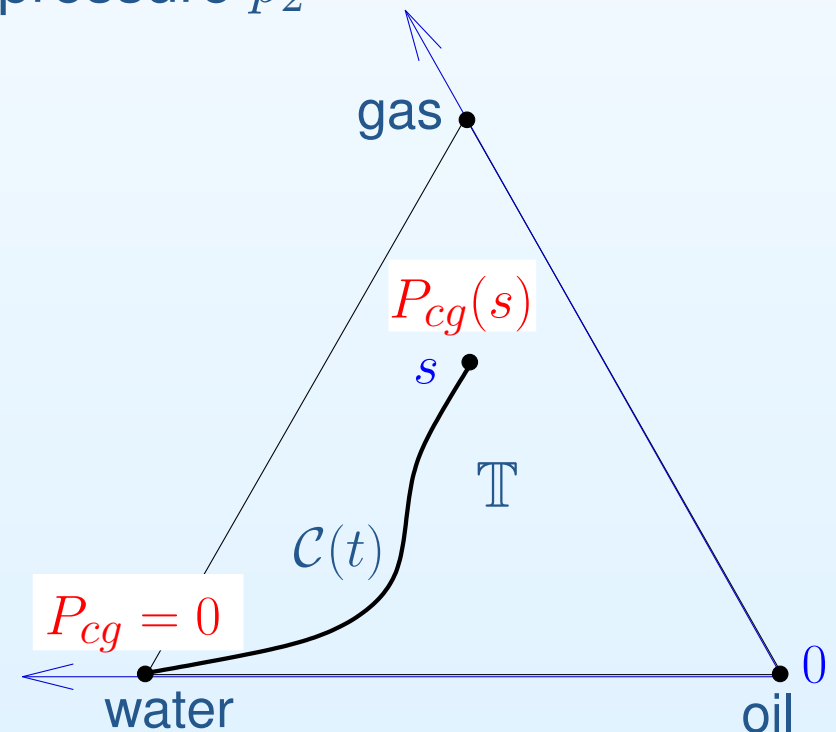
- Condition  $p_1 \leq p \leq p_3$  is satisfied if :

$$P_{cg}(1, 0, p) = 0$$

- When  $P_{cg}$  exists, necessarily

$$P_{cg}(s) = 0 + \int_0^1 \nabla_s P_{cg}(C(t)) \cdot C'(t) dt$$

is independant of  $C$  !



# Total Differential Condition (GC, Applicable Analysis 2009)

- There exists a **Global Capillary Pressure function**  $P_{cg}$  s. t. :

$$\left\{ \begin{array}{l} \frac{\partial P_{cg}}{\partial S_1}(s_1, s_3, p) = f_1(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{12}}{dS_1}(s_1), \\ \frac{\partial P_{cg}}{\partial S_3}(s_1, s_3, p) = f_3(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{32}}{dS_3}(s_3), \end{array} \right.$$

for  $P_{\min} \leq p \leq P_{\max}$ ,  $s = (s_1, s_3) \in \mathbb{T}$ .

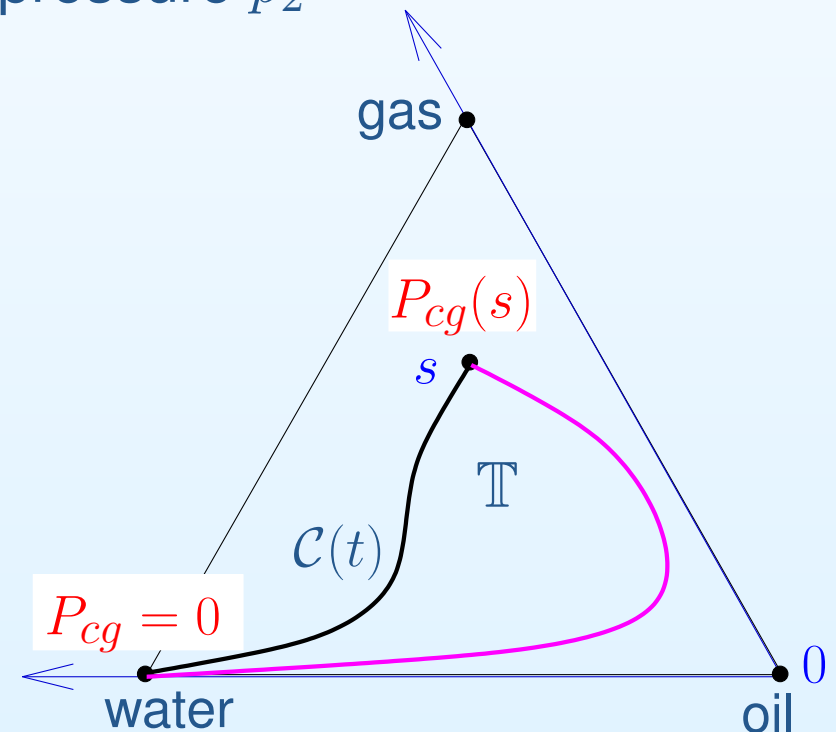
- Condition  $p_1 \leq p \leq p_3$  is satisfied if :

$$P_{cg}(1, 0, p) = 0$$

- When  $P_{cg}$  exists, necessarily

$$P_{cg}(s) = 0 + \int_0^1 \nabla_s P_{cg}(\mathcal{C}(t)) \cdot \mathcal{C}'(t) dt$$

is independant of  $\mathcal{C}$  !



# Total Differential Condition (GC, Applicable Analysis 2009)

- There exists a **Global Capillary Pressure function**  $P_{cg}$  s. t. :

$$\left\{ \begin{array}{l} \frac{\partial P_{cg}}{\partial S_1}(s_1, s_3, p) = f_1(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{12}}{dS_1}(s_1), \\ \frac{\partial P_{cg}}{\partial S_3}(s_1, s_3, p) = f_3(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{32}}{dS_3}(s_3), \end{array} \right.$$

for  $P_{\min} \leq p \leq P_{\max}$ ,  $s = (s_1, s_3) \in \mathbb{T}$ .

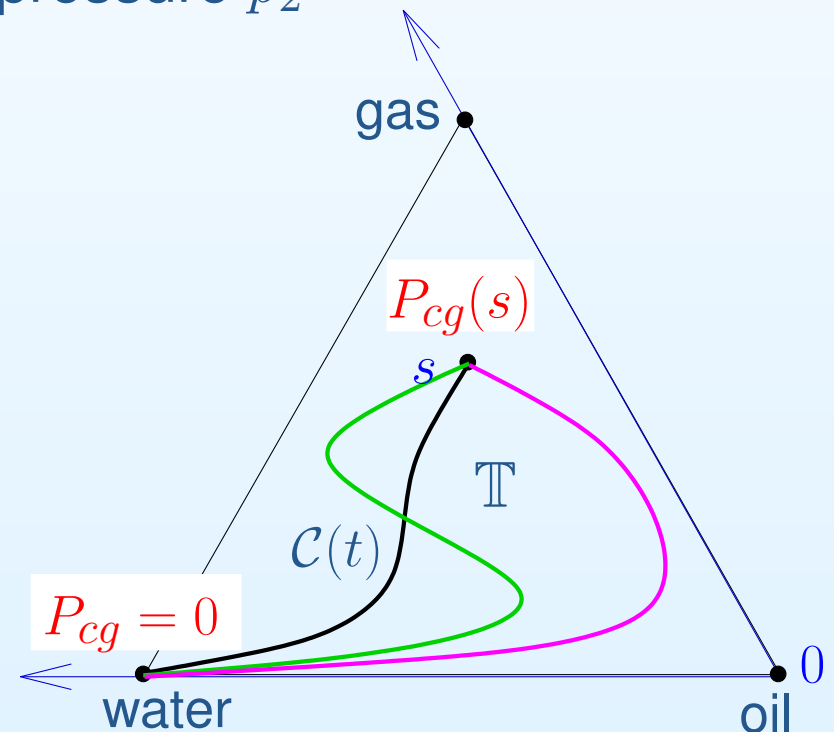
- Condition  $p_1 \leq p \leq p_3$  is satisfied if :

$$P_{cg}(1, 0, p) = 0$$

- When  $P_{cg}$  exists, necessarily

$$P_{cg}(s) = 0 + \int_0^1 \nabla_s P_{cg}(C(t)) \cdot C'(t) dt$$

is independant of  $C$  !



# Total Differential Condition (GC, Applicable Analysis 2009)

- There exists a **Global Capillary Pressure function**  $P_{cg}$  s. t. :

$$\left\{ \begin{array}{l} \frac{\partial P_{cg}}{\partial S_1}(s_1, s_3, p) = f_1(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{12}}{dS_1}(s_1), \\ \frac{\partial P_{cg}}{\partial S_3}(s_1, s_3, p) = f_3(s_1, s_3, \underbrace{p - P_{cg}(s_1, s_3, p)}_{\text{oil pressure } p_2}) \frac{dP_c^{32}}{dS_3}(s_3), \end{array} \right.$$

for  $P_{\min} \leq p \leq P_{\max}$ ,  $s = (s_1, s_3) \in \mathbb{T}$ .

- Condition  $p_1 \leq p \leq p_3$  is satisfied if :

$$P_{cg}(1, 0, p) = 0$$

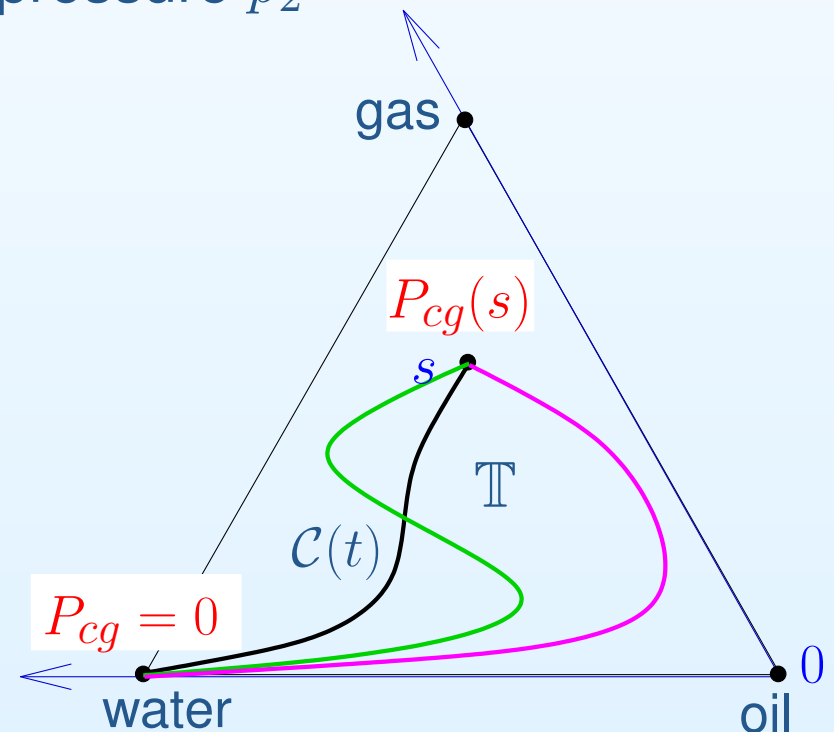
- When  $P_{cg}$  exists, necessarily

$$P_{cg}(s) = 0 + \int_0^1 \nabla_s P_{cg}(C(t)) \cdot C'(t) dt$$

is independant of  $C$  !



**TD-condition** on  $kr_1, kr_2, kr_3, P_c^{12}, P_c^{32}$





## Global pressure formulation :

---

- When  $P_{cg}$  exists, the Global Pressure  $P$  is defined by :

$$P - P_2 = P_{cg}(s, P)$$

- $P$  governs the global flow  $q$  :

$$q = -Kd(s_1, s_3, P) \{ (1 - \partial P_{cg} / \partial P) \nabla P - \rho g \nabla Z \}$$

## Global pressure formulation :

- When  $P_{cg}$  exists, the **Global Pressure**  $P$  is defined by :

$$P - P_2 = P_{cg}(s, P)$$

- $P$  governs the **global flow**  $q$  :

$$q = -Kd(s_1, s_3, P) \{ (1 - \partial P_{cg} / \partial P) \nabla P - \rho g \nabla Z \}$$

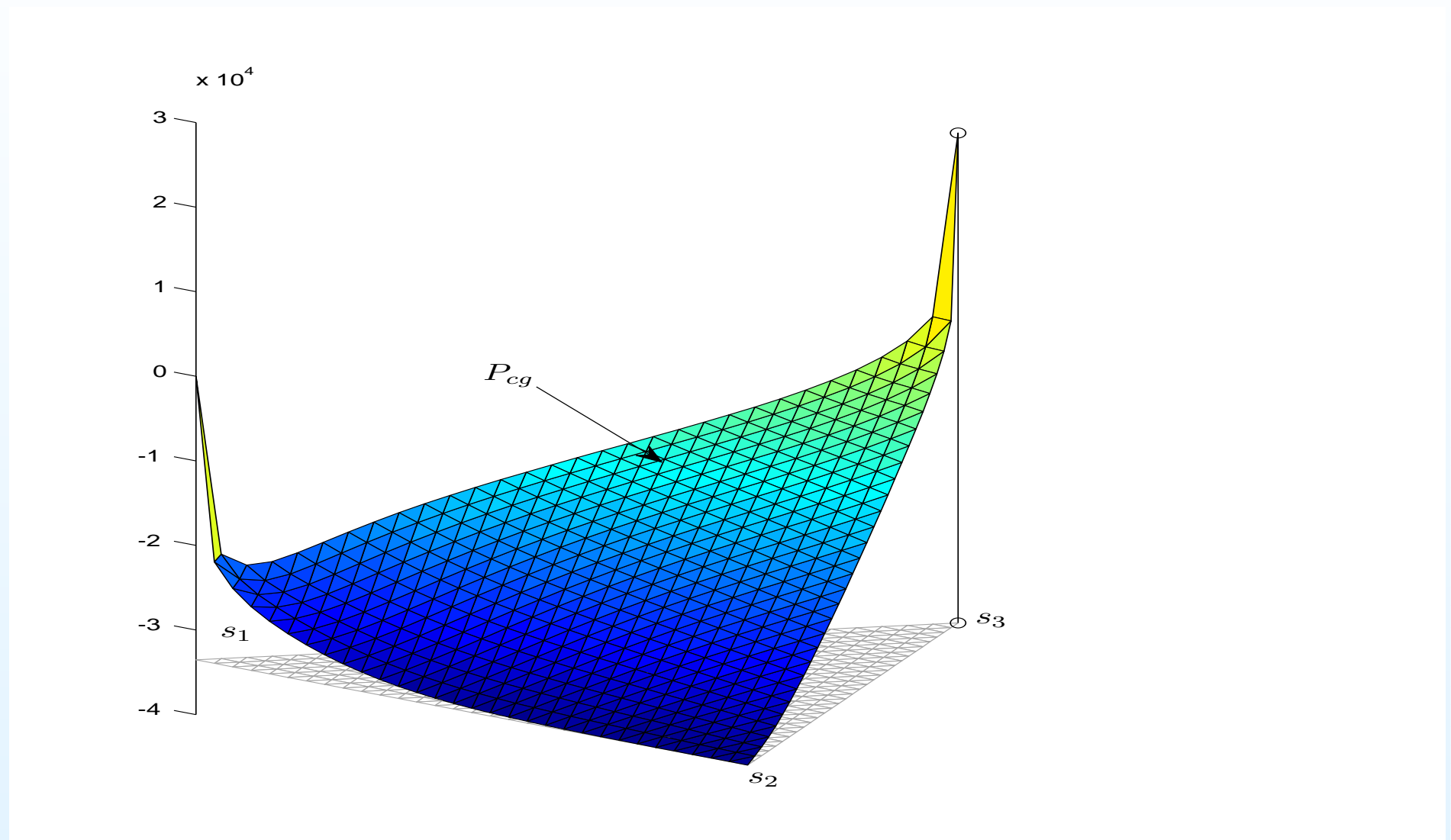
- For a single compressible fluid (gas), one has: :

$$0 < \partial P_{cg} / \partial P \leq 1 \quad \text{over } \mathbb{T}$$

- Numerical results show that:

$$0 < \partial P_{cg} / \partial P \leq 10^{-4} \quad \text{hence :} \quad 1 - \partial P_{cg} / \partial P \simeq 1$$

# Global Capillary Pressure function $P_{cg} = P - P_2$



## Degrees of freedom for TD relative permeabilities :

---

At each global pressure level  $p$

- one can choose freely **only two** functions over  $\mathbb{T}$  :

$$\begin{array}{ll} s \in \mathbb{T} \rightsquigarrow P_{cg}(s, p) & \text{global capillary pressure function} \\ s \in \mathbb{T} \rightsquigarrow d(s, p) & \text{global mobility function} \end{array}$$

## Degrees of freedom for TD relative permeabilities :

---

At each global pressure level  $p$

- one can choose freely **only two** functions over  $\mathbb{T}$  :

$s \in \mathbb{T} \rightsquigarrow P_{cg}(s, p)$       global capillary pressure function

$s \in \mathbb{T} \rightsquigarrow d(s, p)$       global mobility function

- then associated **TD fractional flows** are given by :

$$f_j(s, p) = \partial P_{cg} / \partial s_j(s, p) / dP_c^{j2} / ds_j(s_j) \quad , \quad j = 1, 3$$

## Degrees of freedom for TD relative permeabilities :

At each global pressure level  $p$

- one can choose freely **only two** functions over  $\mathbb{T}$  :

$s \in \mathbb{T} \rightsquigarrow P_{cg}(s, p)$       global capillary pressure function

$s \in \mathbb{T} \rightsquigarrow d(s, p)$       global mobility function

- then associated **TD fractional flows** are given by :

$$f_j(s, p) = \partial P_{cg} / \partial s_j(s, p) / dP_c^{j2} / ds_j(s_j) \quad , \quad j = 1, 3$$

- and associated **TD relative permeabilities** by :

$$\begin{cases} kr_j(s, p) & = f_j(s, p) d(s, p) / d_j(p - P_{cg}(s, p) + P_c^{j2}(s_j)) \quad j = 1, 3 , \\ kr_2(s, p) & = (1 - f_1(s, p) - f_3(s, p)) d(s, p) / d_2(p - P_{cg}(s, p)) , \end{cases}$$

## Construction of TD-relative permeabilities

---

Available experimental data :

- for each fluid  $j = 1, 2, 3$  :

mobilities  $d_j(p_j) = B_j(p_j)/\mu_j(p_j)$  ,

gas



water



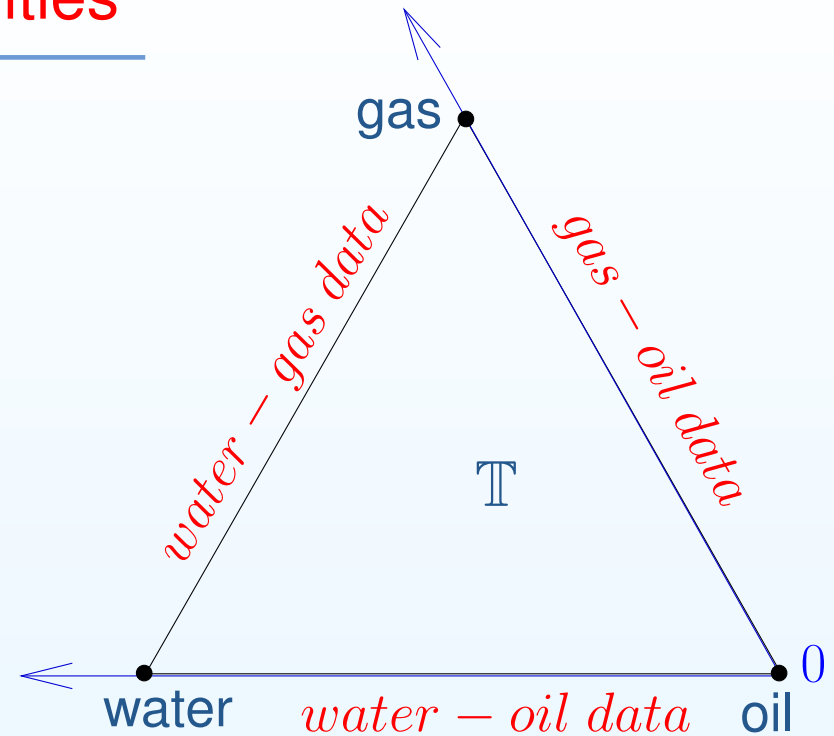
oil



## Construction of TD-relative permeabilities

### Available experimental data :

- for each fluid  $j = 1, 2, 3$  :  
mobilities  $d_j(p_j) = B_j(p_j)/\mu_j(p_j)$  ,
- for each pair of fluids  $i, j$  :

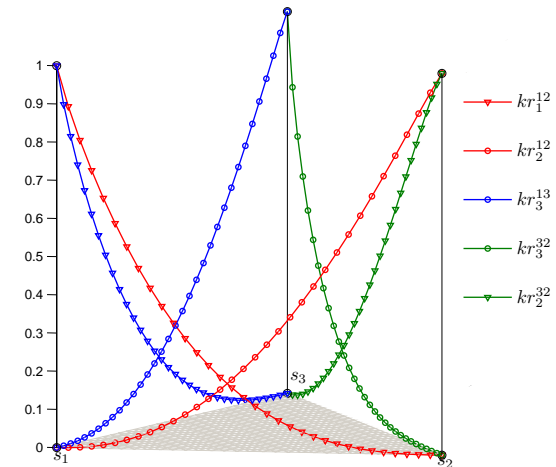




# Construction of TD-relative permeabilities

## Available experimental data :

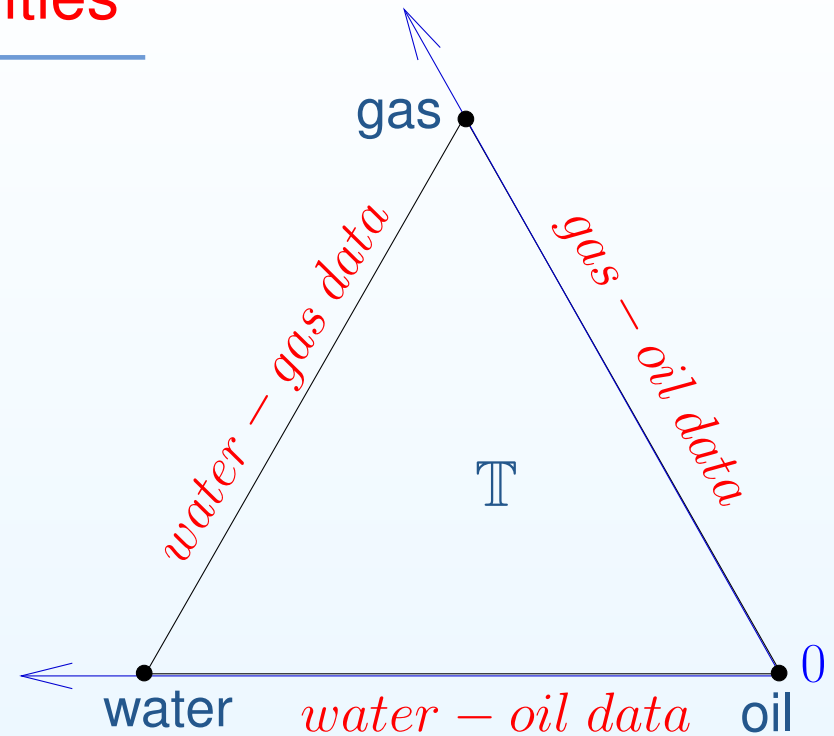
- for each fluid  $j = 1, 2, 3$  :  
mobilities  $d_j(p_j) = B_j(p_j)/\mu_j(p_j)$  ,
- for each pair of fluids  $i, j$  :  
relative permeabilities  $kr_i^{i,j}$  ,  $kr_j^{i,j}$   
(Mualem-Van Genuchten)



## Construction of TD-relative permeabilities

### Available experimental data :

- for each fluid  $j = 1, 2, 3$  :  
mobilities  $d_j(p_j) = B_j(p_j)/\mu_j(p_j)$  ,
- for each pair of fluids  $i, j$  :  
relative permeabilities  $kr_i^{i,j}$  ,  $kr_j^{i,j}$   
(Mualem-Van Genuchten)
- little known on the  $kr$ 's inside  $\mathbb{T}$  !



## Construction of TD-relative permeabilities

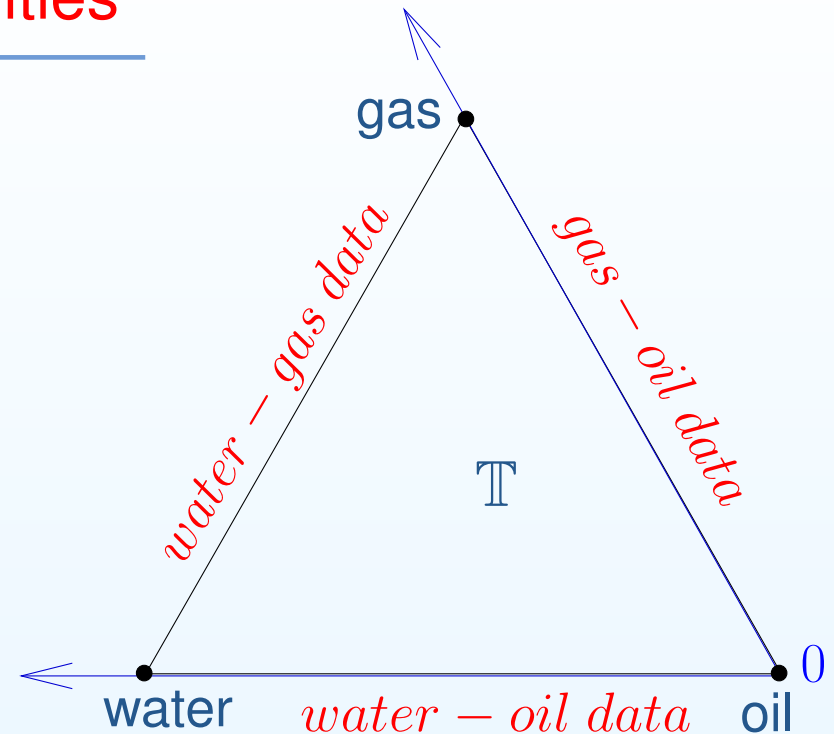
### Available experimental data :

- for each fluid  $j = 1, 2, 3$  :  
mobilities  $d_j(p_j) = B_j(p_j)/\mu_j(p_j)$  ,
- for each pair of fluids  $i, j$  :  
relative permeabilities  $kr_i^{i,j}$  ,  $kr_j^{i,j}$   
(Mualem-Van Genuchten)
- little known on the  $kr$ 's inside  $\mathbb{T}$  !

### Question :

can TD-three-phase relative permeabilities on  $\mathbb{T}$

honor two-phase data on  $\partial\mathbb{T}$  ?

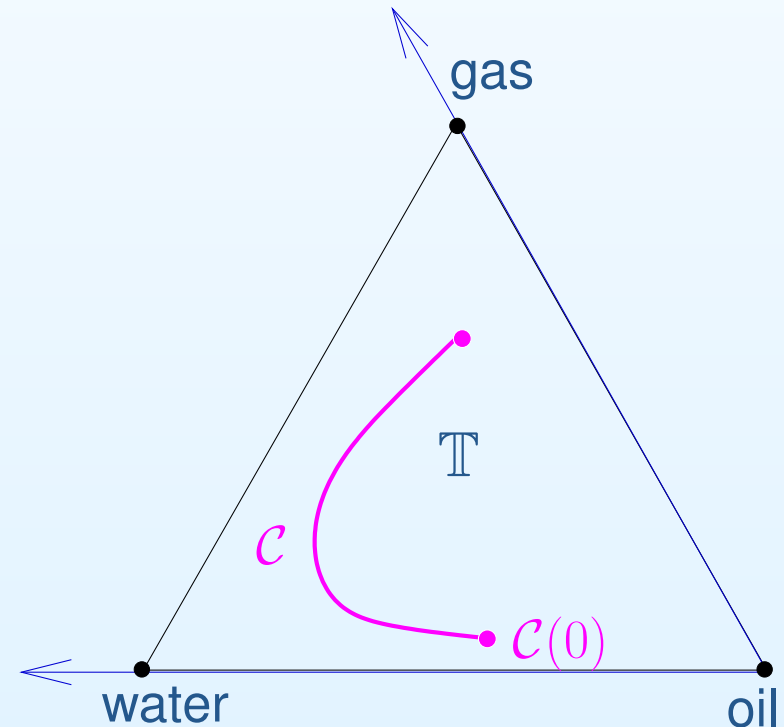


## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Recall : on any curve  $\mathcal{C} : [0, 1] \rightsquigarrow \mathbb{T}$ ,  $P_{cg}(\mathcal{C}(t))$  satisfies :

$$(1) \frac{dP_{cg}}{dt} = f_1(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{12}}{ds_1}(\mathcal{C}_1) \mathcal{C}'_1 + f_3(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{32}}{ds_3}(\mathcal{C}_3) \mathcal{C}'_3 ,$$

- Use (1) to determine of  $P_{cg}$  on  $\partial\mathbb{T}$  :

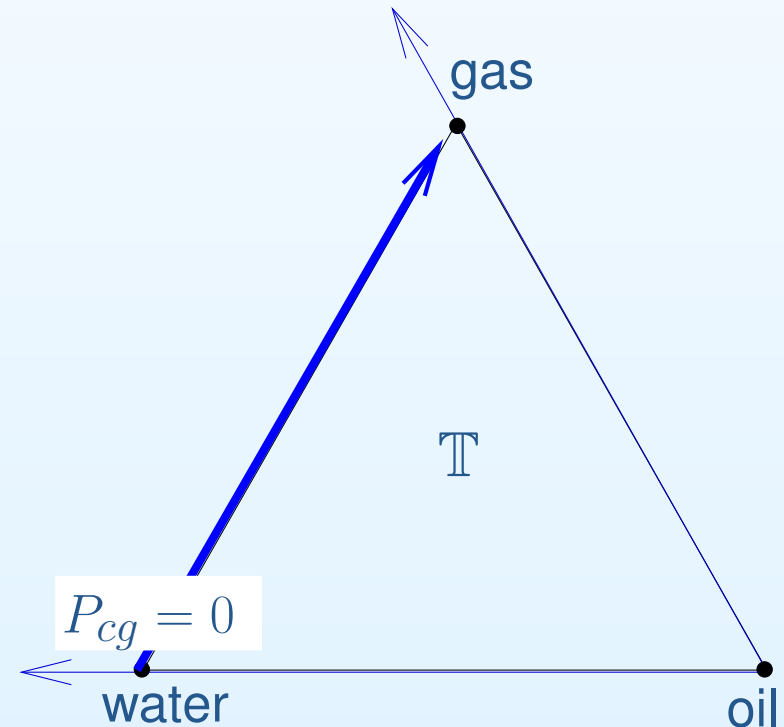


## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Recall : on any curve  $\mathcal{C} : [0, 1] \rightsquigarrow \mathbb{T}$ ,  $P_{cg}(\mathcal{C}(t))$  satisfies :

$$(1) \frac{dP_{cg}}{dt} = f_1(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{12}}{ds_1}(\mathcal{C}_1) \mathcal{C}'_1 + f_3(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{32}}{ds_3}(\mathcal{C}_3) \mathcal{C}'_3 ,$$

- Use (1) to determine of  $P_{cg}$  on  $\partial\mathbb{T}$  :  
 - on the **water-gas** side  $\implies P_{cg}^{13}$

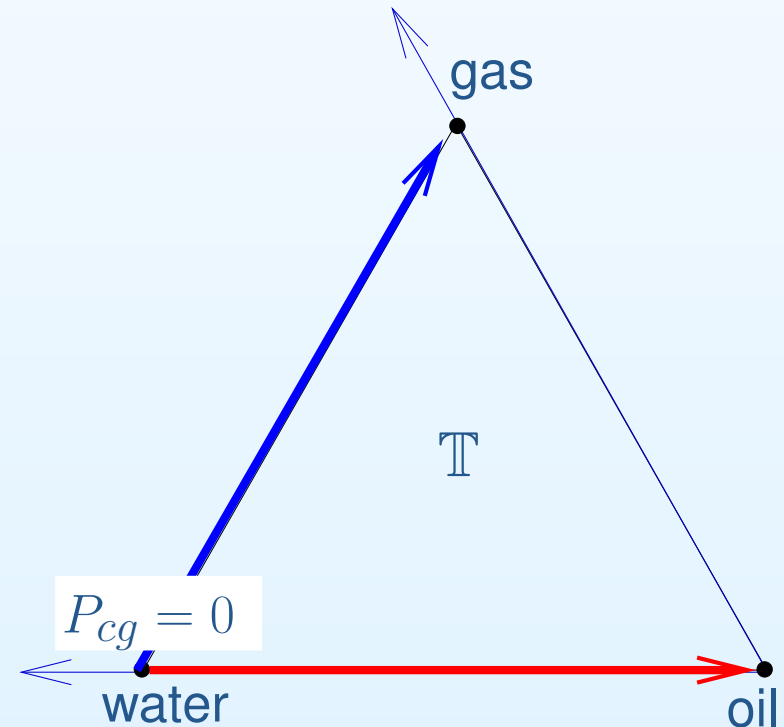


## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Recall : on any curve  $\mathcal{C} : [0, 1] \rightsquigarrow \mathbb{T}$ ,  $P_{cg}(\mathcal{C}(t))$  satisfies :

$$(1) \frac{dP_{cg}}{dt} = f_1(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{12}}{ds_1}(\mathcal{C}_1) \mathcal{C}'_1 + f_3(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{32}}{ds_3}(\mathcal{C}_3) \mathcal{C}'_3 ,$$

- Use (1) to determine of  $P_{cg}$  on  $\partial\mathbb{T}$  :
  - on the **water-gas** side  $\implies P_{cg}^{13}$
  - on the **water-oil** side  $\implies P_{cg}^{12}$

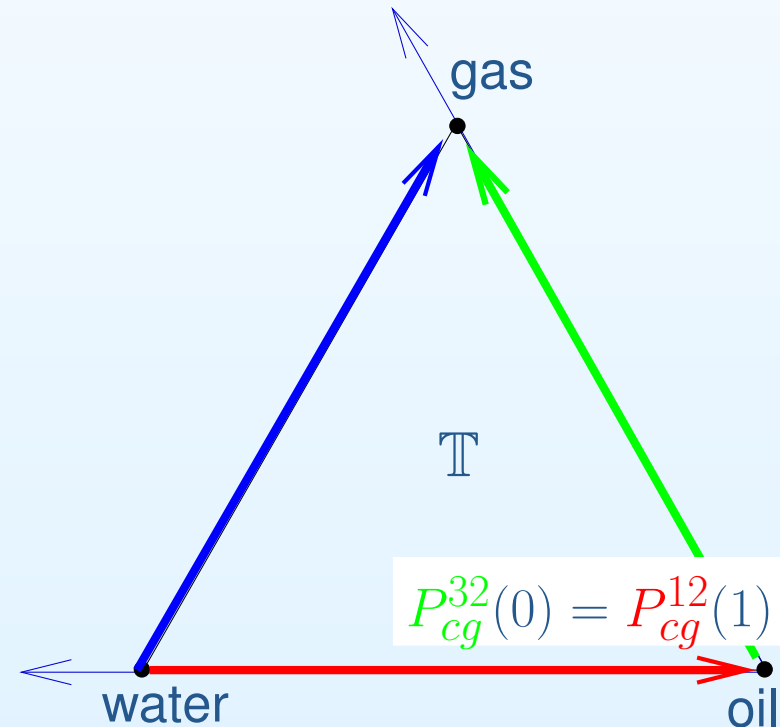


## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Recall : on any curve  $\mathcal{C} : [0, 1] \rightsquigarrow \mathbb{T}$ ,  $P_{cg}(\mathcal{C}(t))$  satisfies :

$$(1) \frac{dP_{cg}}{dt} = f_1(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{12}}{ds_1}(\mathcal{C}_1) \mathcal{C}'_1 + f_3(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{32}}{ds_3}(\mathcal{C}_3) \mathcal{C}'_3 ,$$

- Use (1) to determine of  $P_{cg}$  on  $\partial\mathbb{T}$  :
  - on the **water-gas** side  $\implies P_{cg}^{13}$
  - on the **water-oil** side  $\implies P_{cg}^{12}$
  - on the **gas-oil** side  $\implies P_{cg}^{23}$



## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Recall : on any curve  $\mathcal{C} : [0, 1] \rightsquigarrow \mathbb{T}$ ,  $P_{cg}(\mathcal{C}(t))$  satisfies :

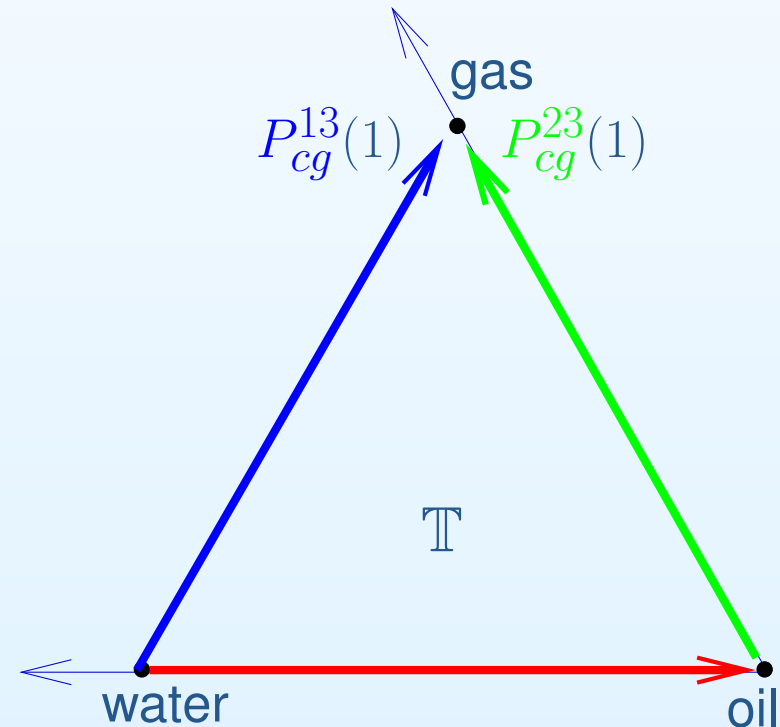
$$(1) \frac{dP_{cg}}{dt} = f_1(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{12}}{ds_1}(\mathcal{C}_1) \mathcal{C}'_1 + f_3(\mathcal{C}, \underbrace{p - P_{cg}}_{P_2}) \frac{dP_c^{32}}{ds_3}(\mathcal{C}_3) \mathcal{C}'_3 ,$$

- Use (1) to determine of  $P_{cg}$  on  $\partial\mathbb{T}$  :

- on the **water-gas** side  $\implies P_{cg}^{13}$
- on the **water-oil** side  $\implies P_{cg}^{12}$
- on the **gas-oil** side  $\implies P_{cg}^{23}$

- **TD-compatibility condition** for the two-phase  $kr$  data :

$$P_{cg}^{13}(1) = P_{cg}^{23}(1) (= +\infty !)$$





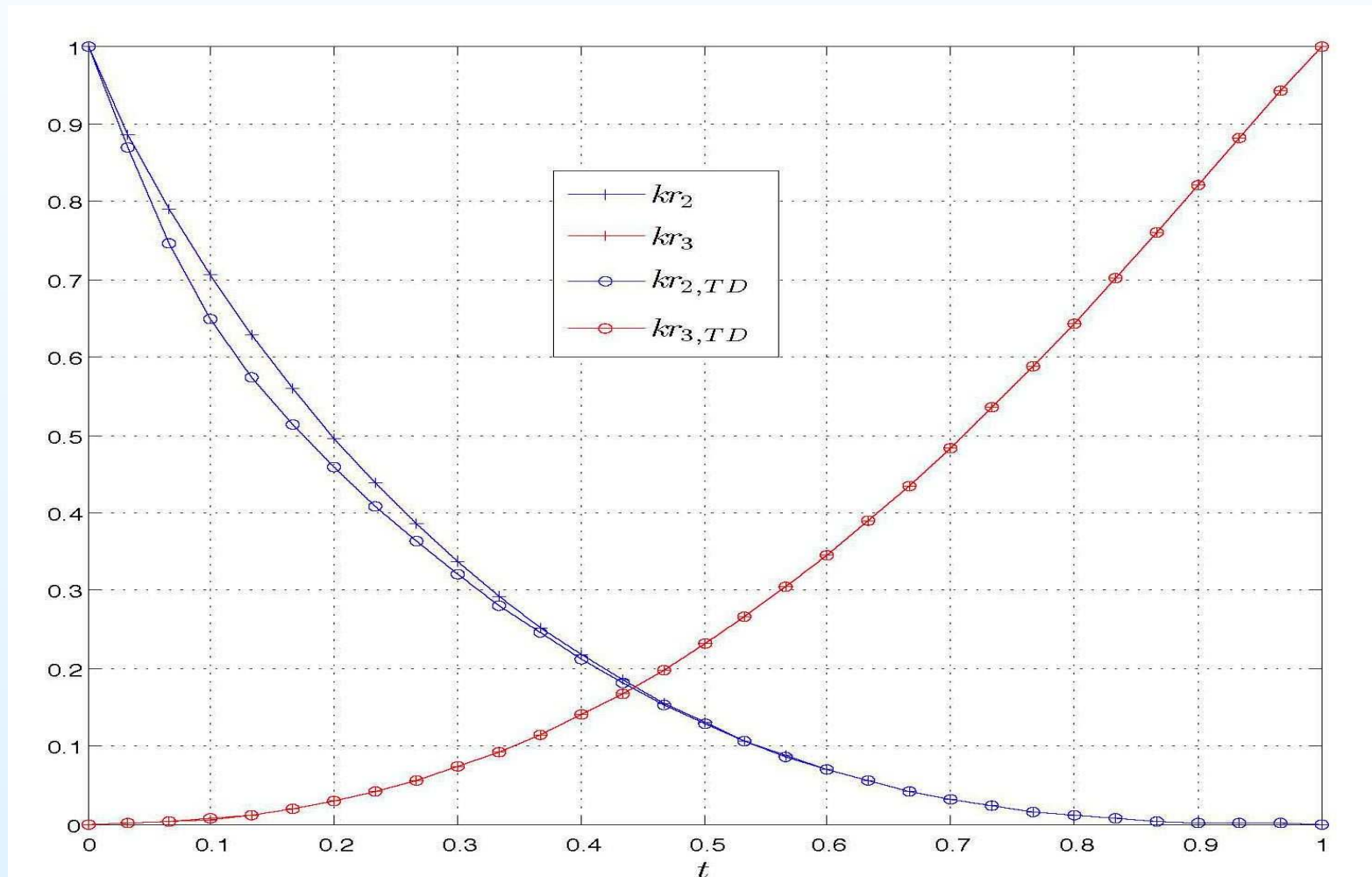
## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial T$

---

- Adjust  $P_{cg}^{32}$  to satisfy the TD-compatibility condition  $P_{cg}^{13}(1) = P_{cg}^{32}(1)$

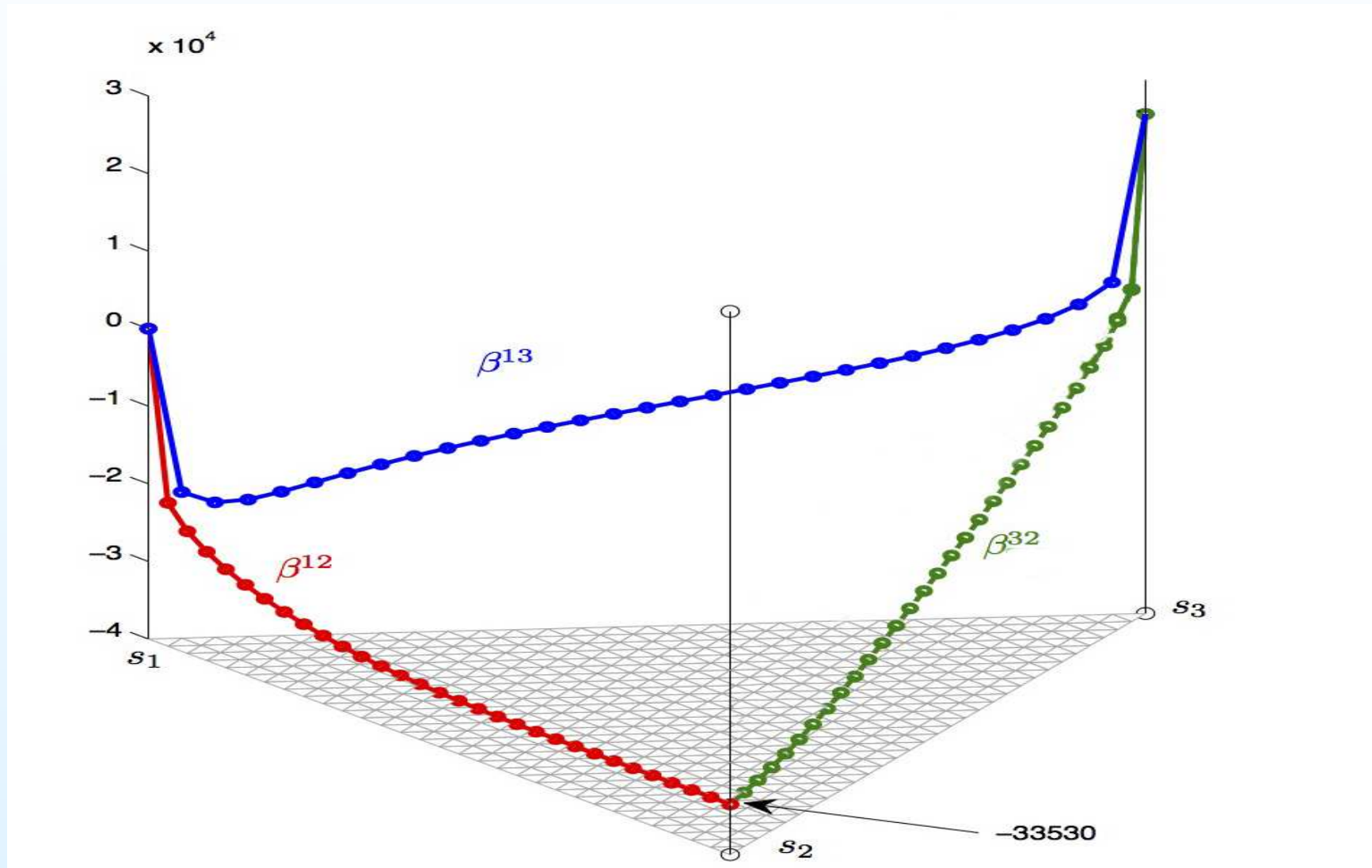
## Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial T$

- Adjust  $P_{cg}^{32}$  to satisfy the TD-compatibility condition  $P_{cg}^{13}(1) = P_{cg}^{32}(1)$
- Implies minor changes on the oil-gas relative permeabilities:



# Honoring two-phase data : 1 Determine $P_{cg}$ on $\partial T$

- now  $P_{cg}$  is available on  $\partial T$  !

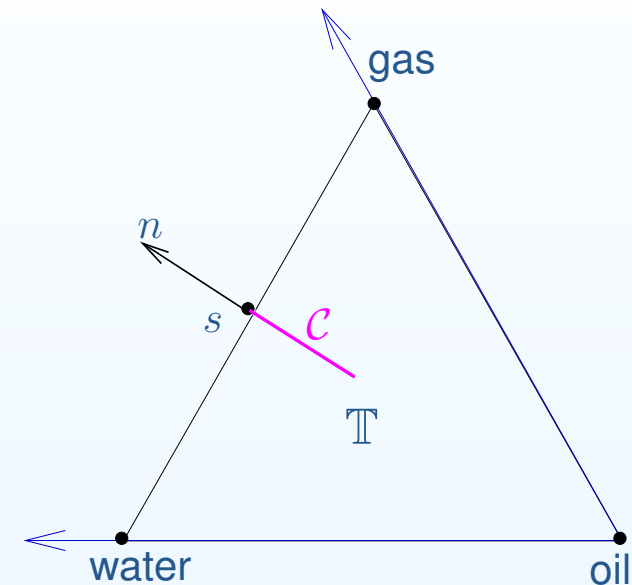


## Honoring two-phase data: 2 determine $\partial P_{cg}/\partial n$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Let  $s \in \partial\mathbb{T}$ ,  $n$  normal to  $\partial\mathbb{T}$  at  $s$ , and define :

$\mathcal{C} : t \in [0, \epsilon] \rightsquigarrow \mathcal{C}(t) = s - tn \in \mathbb{T}$   
a curve normal to  $\partial\mathbb{T}$  at  $s$ .

Then 
$$\frac{\partial P_{cg}}{\partial n}(s) = -\frac{d}{dt} P_{cg}(\mathcal{C}(t))|_{t=0}.$$



## Honoring two-phase data: 2 determine $\partial P_{cg}/\partial n$ on $\partial\mathbb{T}$

- Let  $p$  be a given **global pressure** level.
- Let  $s \in \partial\mathbb{T}$ ,  $n$  normal to  $\partial\mathbb{T}$  at  $s$ , and define :

$C : t \in [0, \epsilon] \rightsquigarrow C(t) = s - tn \in \mathbb{T}$   
 a curve normal to  $\partial\mathbb{T}$  at  $s$ .

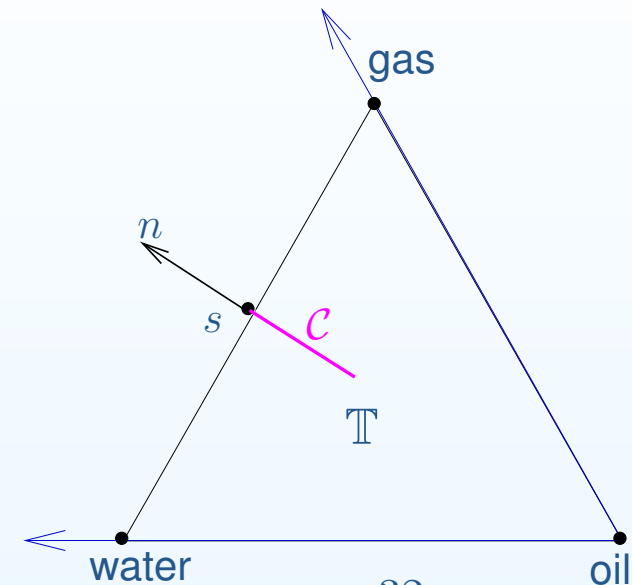
Then  $\frac{\partial P_{cg}}{\partial n}(s) = -\frac{d}{dt} P_{cg}(C(t))|_{t=0}$ .

But using again equation (1) :

$$(1) \frac{dP_{cg}}{dt} = f_1(\underbrace{C, p - P_{cg}}_{P_2}) \frac{dP_c^{12}}{ds_1}(C_1) C'_1 + f_3(\underbrace{C, p - P_{cg}}_{P_2}) \frac{dP_c^{32}}{ds_3}(C_3) C'_3,$$

gives:

$$\frac{\partial P_{cg}}{\partial n} = \begin{cases} \frac{\sqrt{3}}{3} f_1^{12} \frac{dP_c^{12}}{ds_1} & \text{(water-oil edge),} \\ \frac{\sqrt{3}}{3} \left( f_1^{13} \frac{dP_c^{12}}{ds_1} + f_3^{13} \frac{dP_c^{32}}{ds_3} \right) & \text{(water-gas edge),} \\ \frac{\sqrt{3}}{3} f_3^{23} \frac{dP_c^{32}}{ds_3} & \text{(gas oil edge),} \end{cases}$$

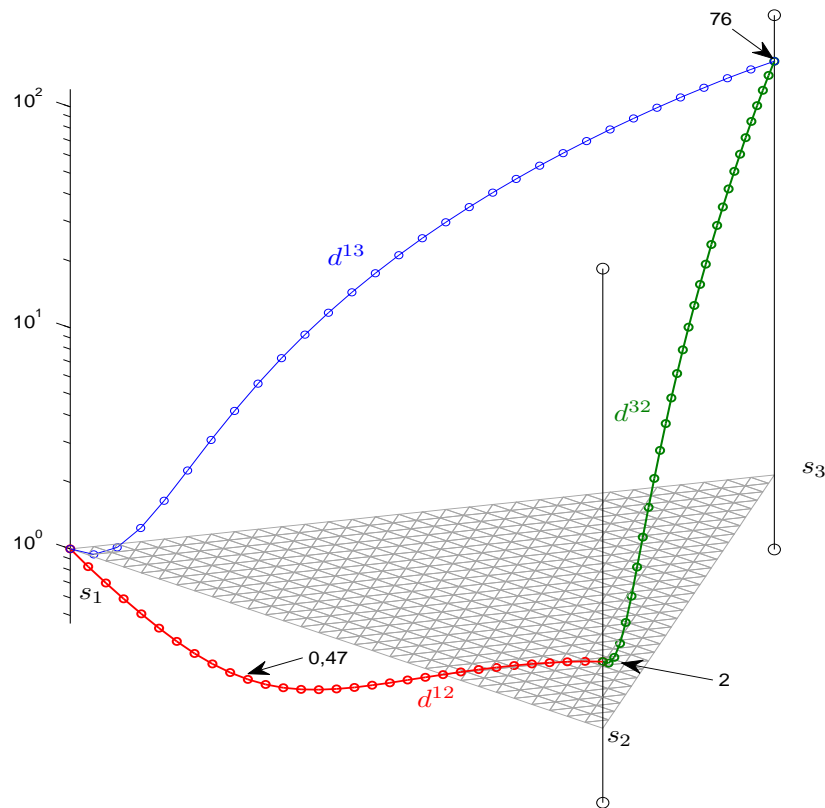


## Honoring two-phase data: 3 determine mobility $d$ on $\partial\mathbb{T}$

$$d = \begin{cases} kr_1 d_1(p - P_{cg}^{12} + P_c^{12}) + kr_2 d_2(p - P_{cg}^{12}) & \text{(water-oil)} \\ kr_1 d_1(p - P_{cg}^{13} + P_c^{12}) + kr_3 d_3(p - P_{cg}^{13} + P_c^{32}) & \text{(gas-water)} \\ kr_3 d_3(p - P_{cg}^{32} + P_c^{32}) + kr_2^{32} d_2(p - P_{cg}^{32}) & \text{(gas-oil)} \end{cases}$$

# Honoring two-phase data: 3 determine mobility $d$ on $\partial\mathbb{T}$

$$d = \begin{cases} kr_1 d_1(p - P_{cg}^{12} + P_c^{12}) + kr_2 d_2(p - P_{cg}^{12}) & \text{(water-oil)} \\ kr_1 d_1(p - P_{cg}^{13} + P_c^{12}) + kr_3 d_3(p - P_{cg}^{13} + P_c^{32}) & \text{(gas-water)} \\ kr_3 d_3(p - P_{cg}^{32} + P_c^{32}) + kr_2^2 d_2(p - P_{cg}^{32}) & \text{(gas-oil)} \end{cases}$$



## Honoring two-phase data: 4 - Find $P_{cg}$ and $d$ inside $\mathbb{T}$

### A - FIRST APPROACH : INTERPOLATION

- Harmonic for  $d$  and Biharmonic for  $P_{cg}$  :

$$\left\{ \begin{array}{l} -\Delta d = 0 \\ d = d^{data} \end{array} \right. \text{ in } \mathbb{T}, \text{ on } \partial\mathbb{T} . \quad \left\{ \begin{array}{l} \Delta^2 P_{cg} = 0 \\ P_{cg} = P_{cg}^{data} \\ \frac{\partial P_{cg}}{\partial n} = \frac{\partial P_{cg}^{data}}{\partial n} \end{array} \right. \text{ in } \mathbb{T}, \text{ on } \partial\mathbb{T} .$$



## Honoring two-phase data: 4 - Find $P_{cg}$ and $d$ inside $\mathbb{T}$

### A - FIRST APPROACH : INTERPOLATION

- Harmonic for  $d$  and Biharmonic for  $P_{cg}$  :

$$\left\{ \begin{array}{l} -\Delta d = 0 \\ d = d^{data} \end{array} \right. \text{ in } \mathbb{T}, \text{ on } \partial\mathbb{T} . \quad \left\{ \begin{array}{l} \Delta^2 P_{cg} = 0 \\ P_{cg} = P_{cg}^{data} \\ \frac{\partial P_{cg}}{\partial n} = \frac{\partial P_{cg}^{data}}{\partial n} \end{array} \right. \text{ in } \mathbb{T}, \text{ on } \partial\mathbb{T} .$$

- Finite element parameterization :

reduced HCT for  $P_{cg}$  ,  $P^1$  for  $d$ .

(di Chiara Roupert, Chavent and Schaefer, J. Comp. Physic 2010)

## Honoring two-phase data: 4 - Find $P_{cg}$ and $d$ inside $\mathbb{T}$

### A - FIRST APPROACH : INTERPOLATION

- Harmonic for  $d$  and Biharmonic for  $P_{cg}$  :

$$\left\{ \begin{array}{l} -\Delta d = 0 \\ d = d^{data} \end{array} \right. \text{ in } \mathbb{T}, \text{ on } \partial\mathbb{T} . \quad \left\{ \begin{array}{l} \Delta^2 P_{cg} = 0 \\ P_{cg} = P_{cg}^{data} \\ \frac{\partial P_{cg}}{\partial n} = \frac{\partial P_{cg}^{data}}{\partial n} \end{array} \right. \text{ in } \mathbb{T}, \text{ on } \partial\mathbb{T} .$$

- Finite element parameterization :

reduced HCT for  $P_{cg}$  ,  $P^1$  for  $d$ .

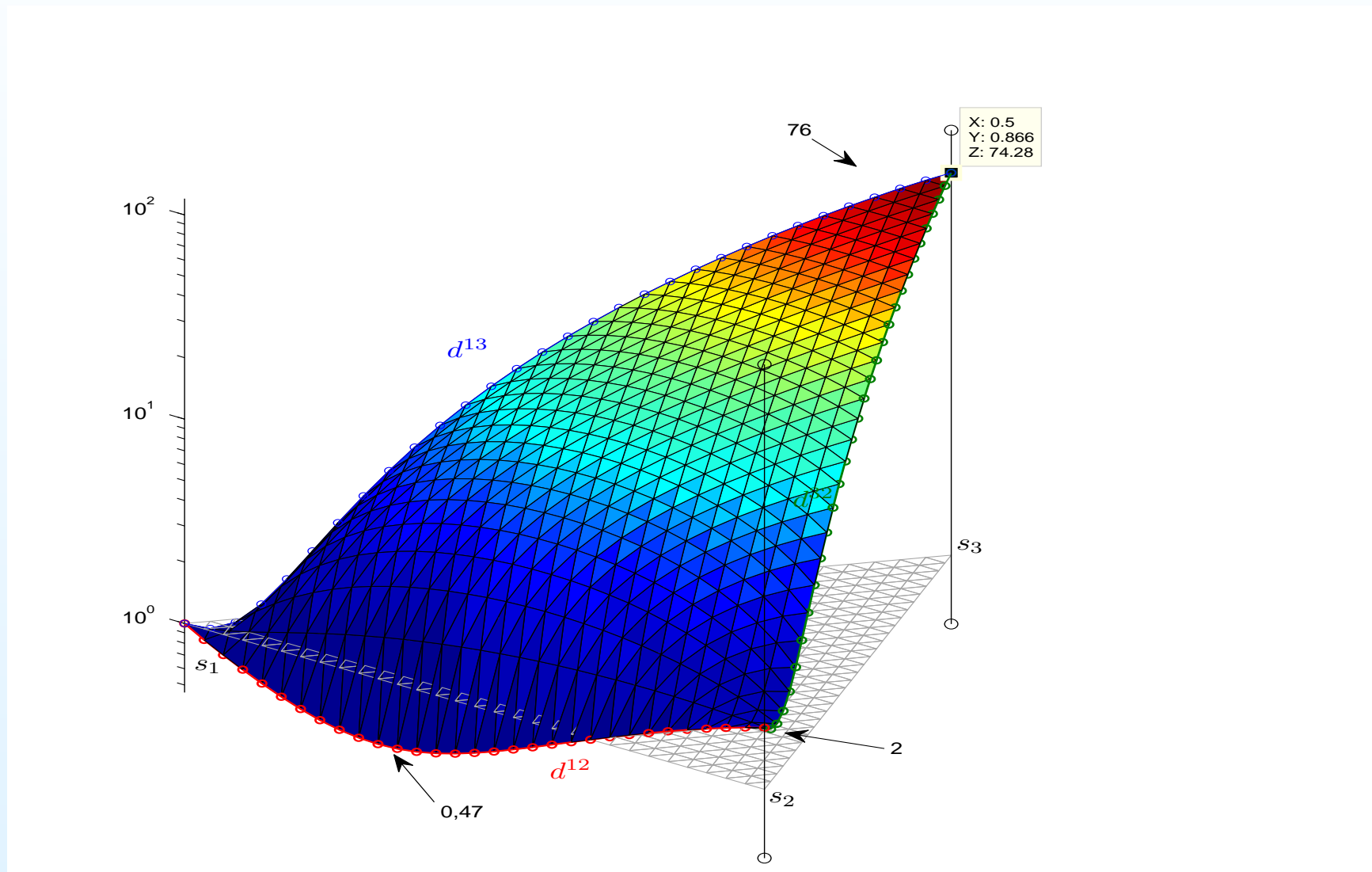
(di Chiara Roupert, Chavent and Schaefer, J. Comp. Physic 2010)

- **Limitations** : no control on relative permeabilities inside  $\mathbb{T}$

### B - SECOND APPROACH : OPTIMIZATION ...still to be tested !

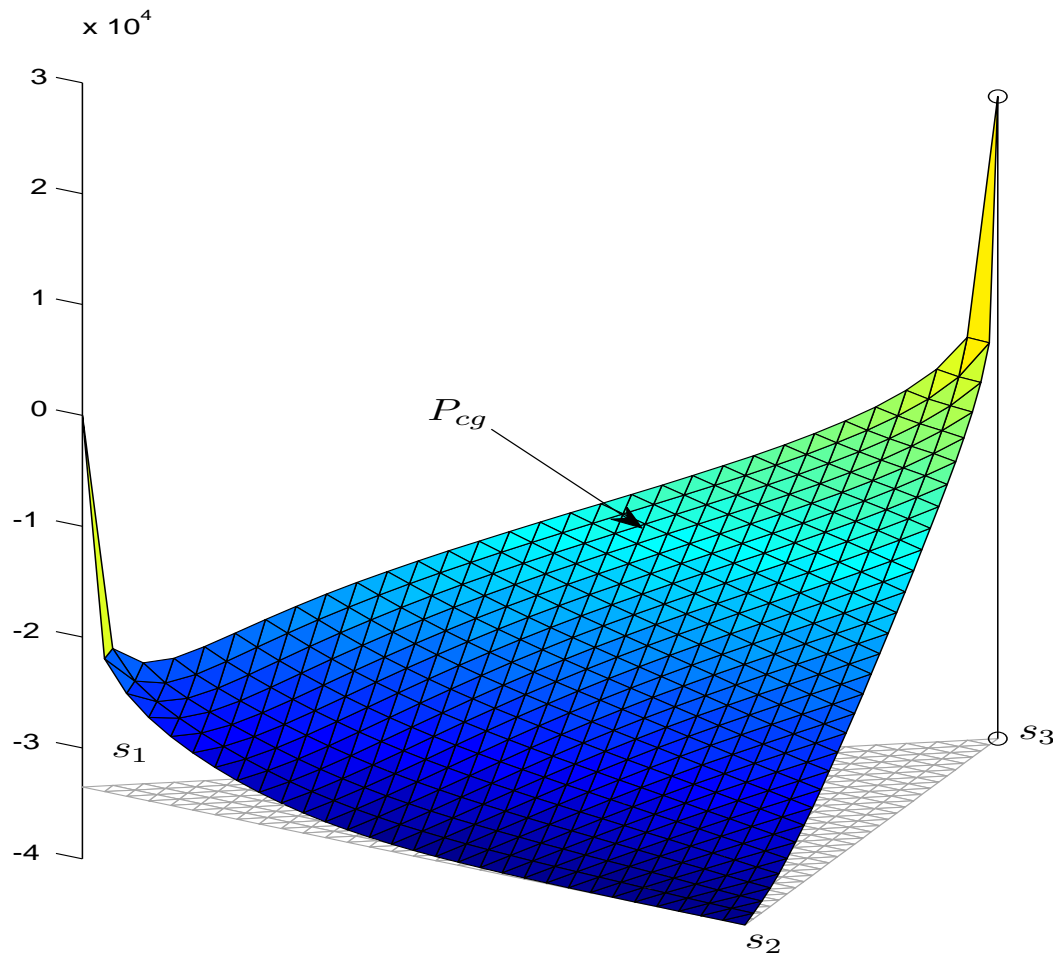
# INTERPOLATION - Numerical results :

- global mobility  $d$  :



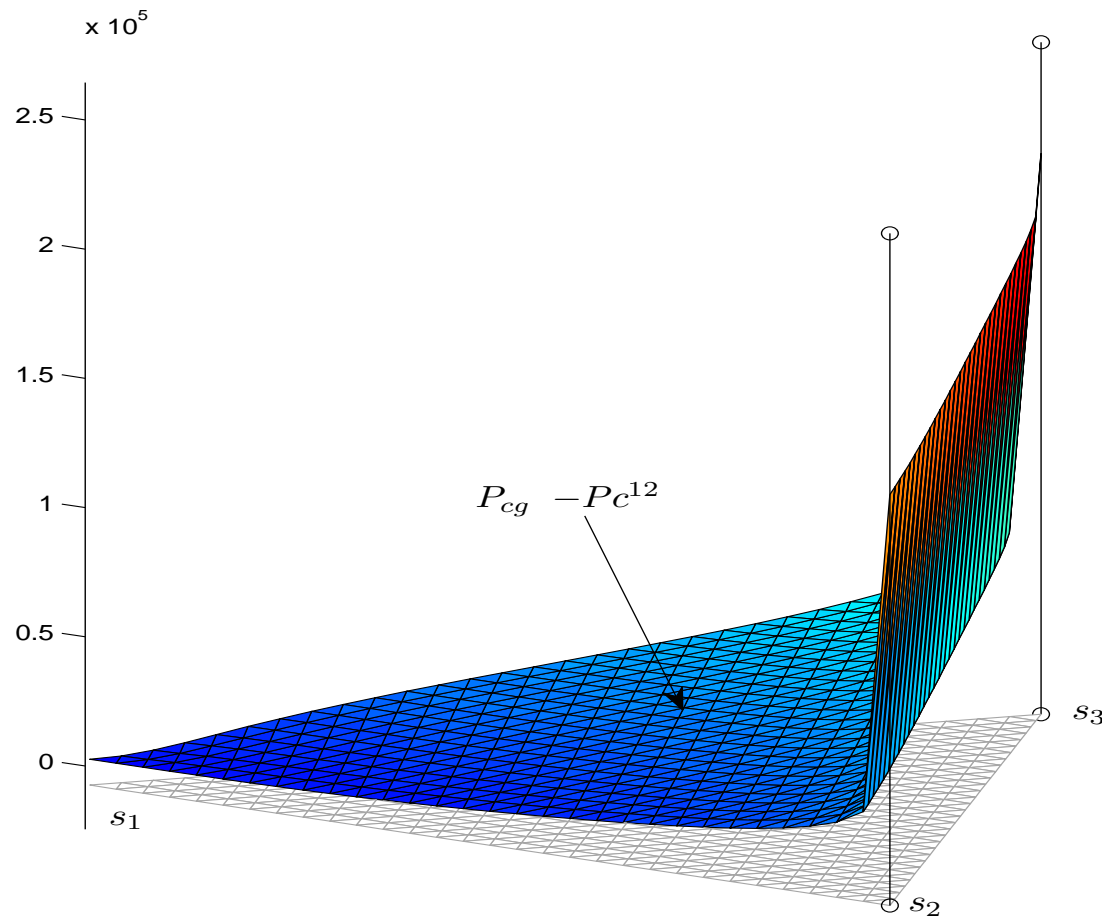
# INTERPOLATION - Numerical results :

- global capillary pressure  $P_{cg} = \text{global pressure } p - \text{oil pressure } p_2$



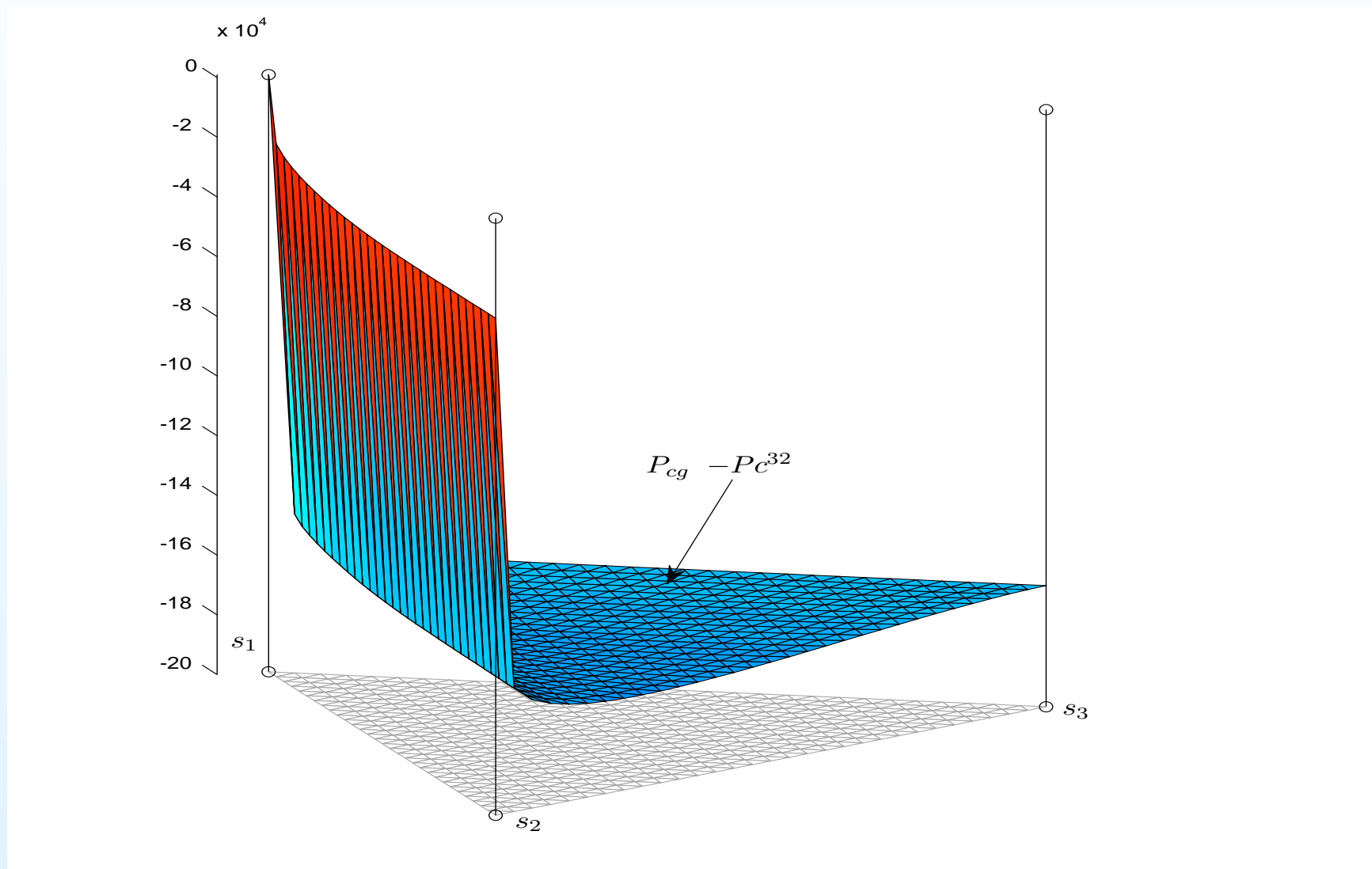
# INTERPOLATION - Numerical results :

- global pressure  $p$  - water pressure  $p_1 = P_{cg} - p_c^{12}$



# INTERPOLATION - Numerical results :

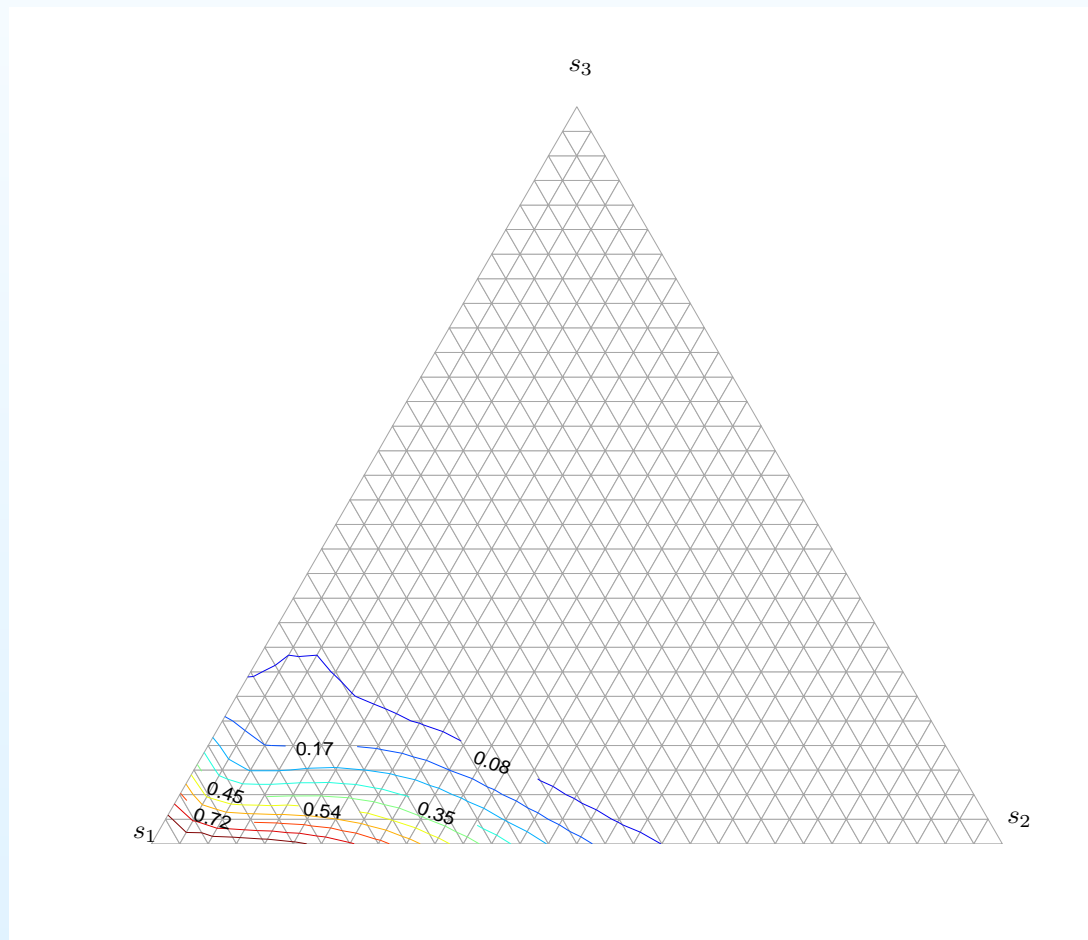
- global pressure  $p$  - gas pressure  $p_3 = P_{cg} - p_c^{32}$



# INTERPOLATION - Back to relative permeabilities :

- **Step 1** :  $P_{cg} \Rightarrow$  TD Three-phase fractional flows

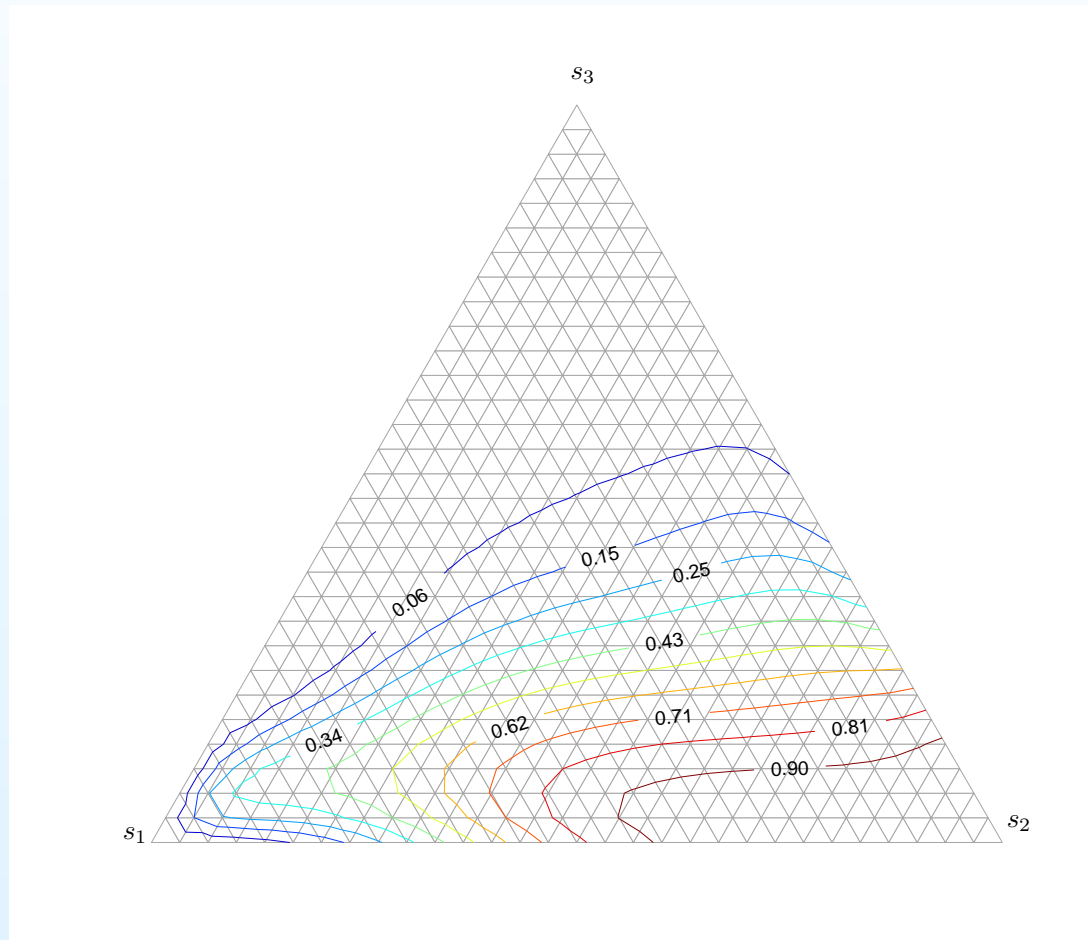
$$\nu_j = \partial P_{cg} / \partial s_j / dP_c^{j2} / ds_j, \quad j = 1, 3, \quad \nu_2 = 1 - \nu_1 - \nu_3$$



# INTERPOLATION - Back to relative permeabilities :

- **Step 1** :  $P_{cg}$   $\Rightarrow$  TD Three-phase fractional flows

$$\nu_j = \partial P_{cg} / \partial s_j / dP_c^{j2} / ds_j , j = 1, 3 \quad , \quad \nu_2 = 1 - \nu_1 - \nu_3$$

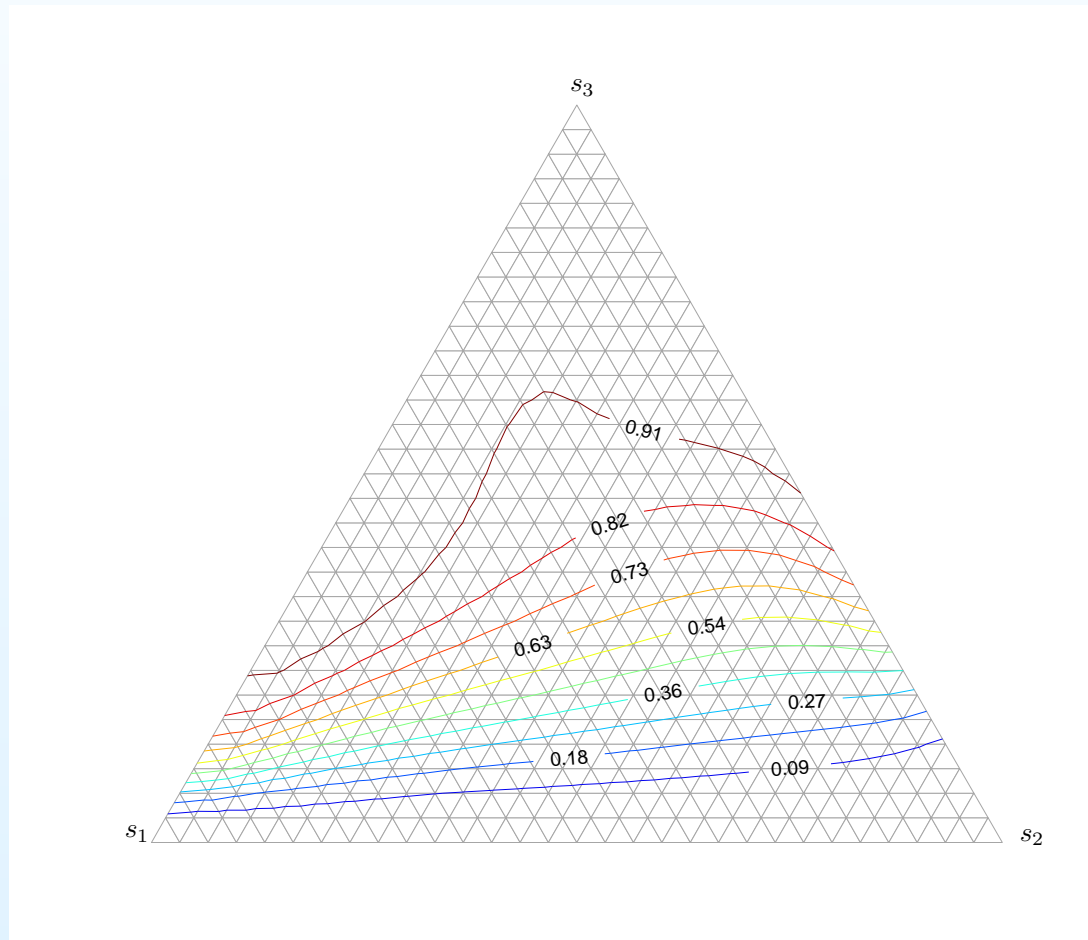




# INTERPOLATION - Back to relative permeabilities :

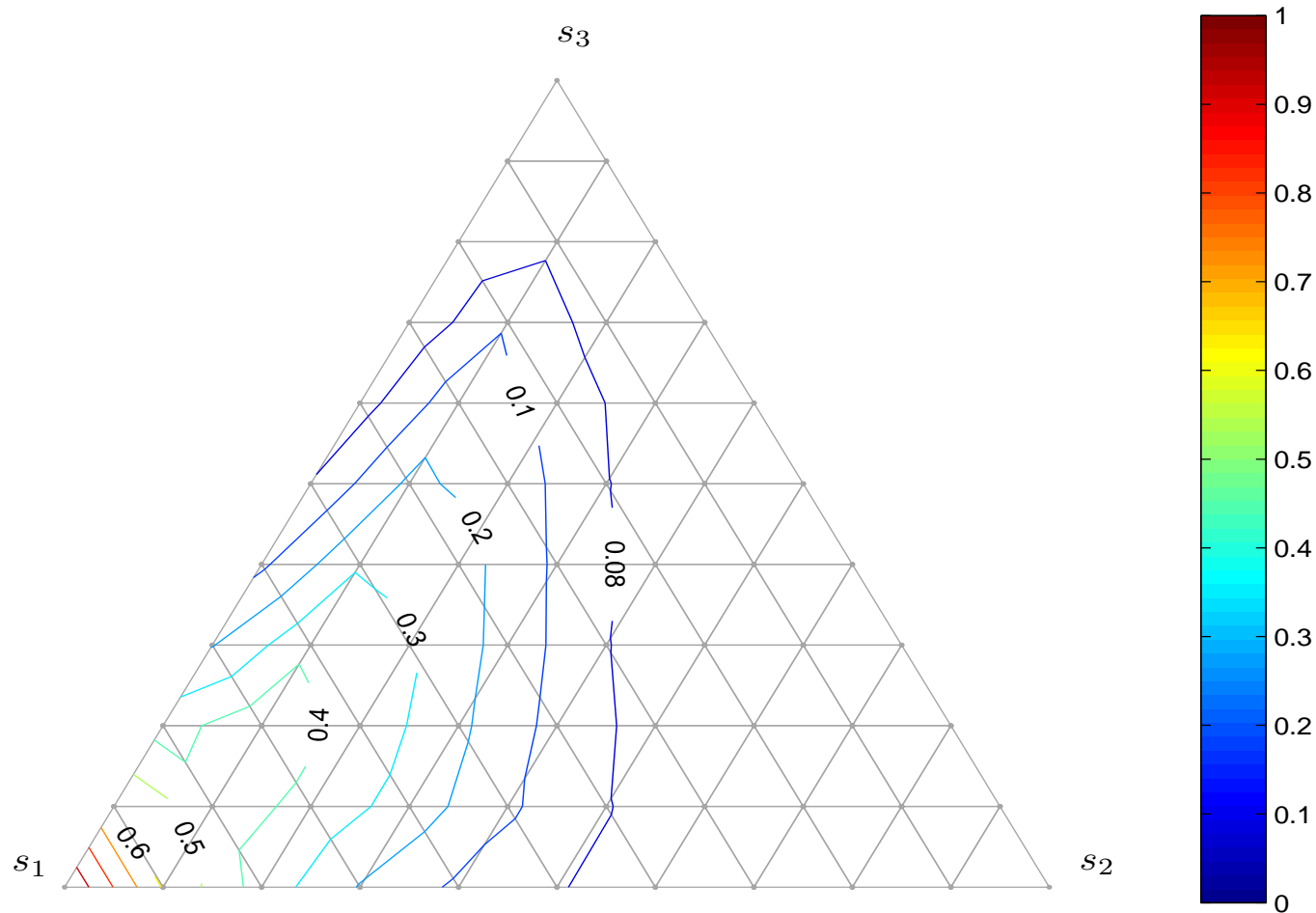
- **Step 1** :  $P_{cg} \Rightarrow$  TD Three-phase fractional flows

$$\nu_j = \partial P_{cg} / \partial s_j / dP_c^{j2} / ds_j, \quad j = 1, 3, \quad \nu_2 = 1 - \nu_1 - \nu_3$$



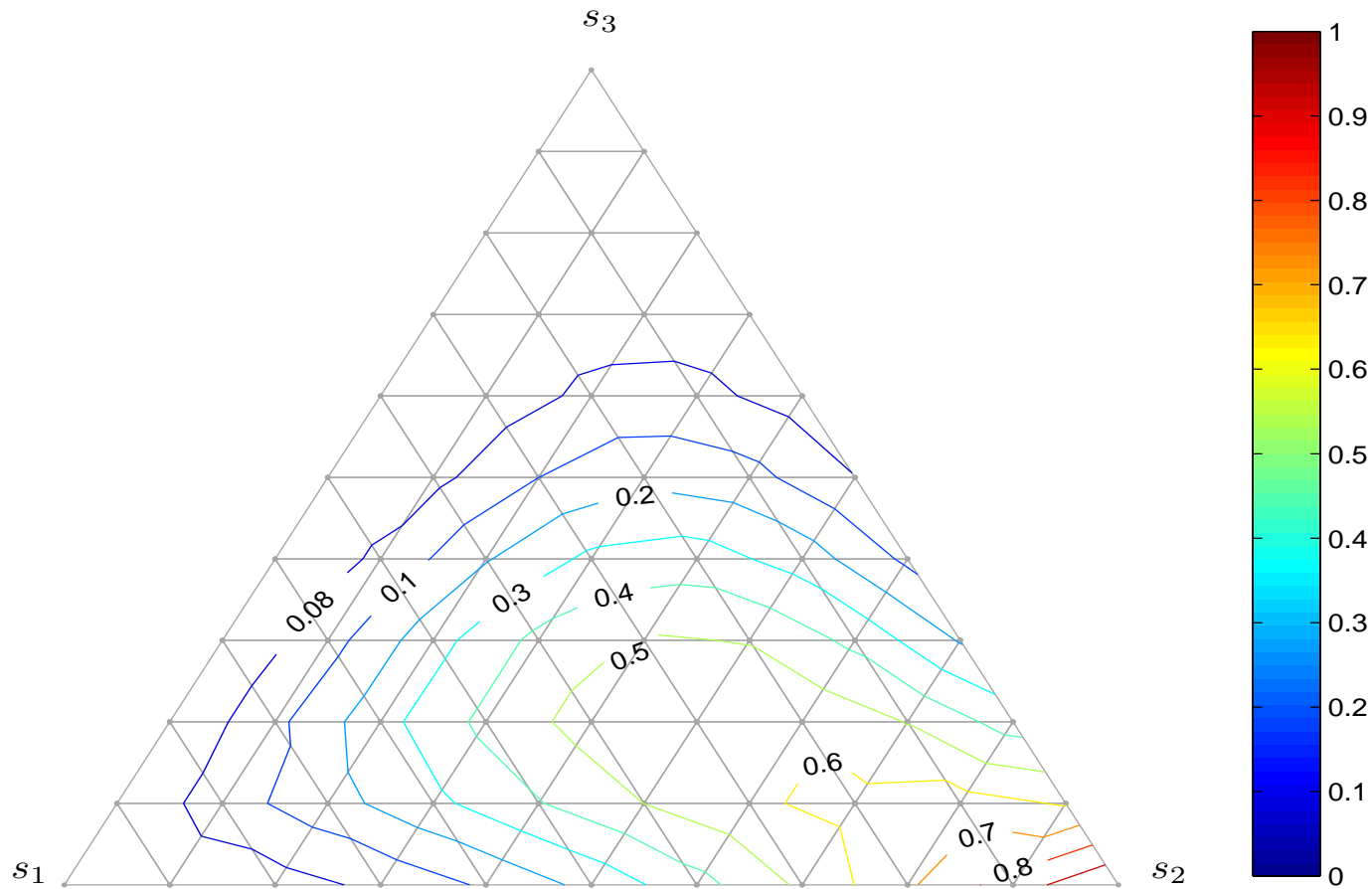
# INTERPOLATION - Back to relative permeabilities :

- Step 2 :  $P_{cg}, d \Rightarrow$  TD Three-phase relative permeabilities



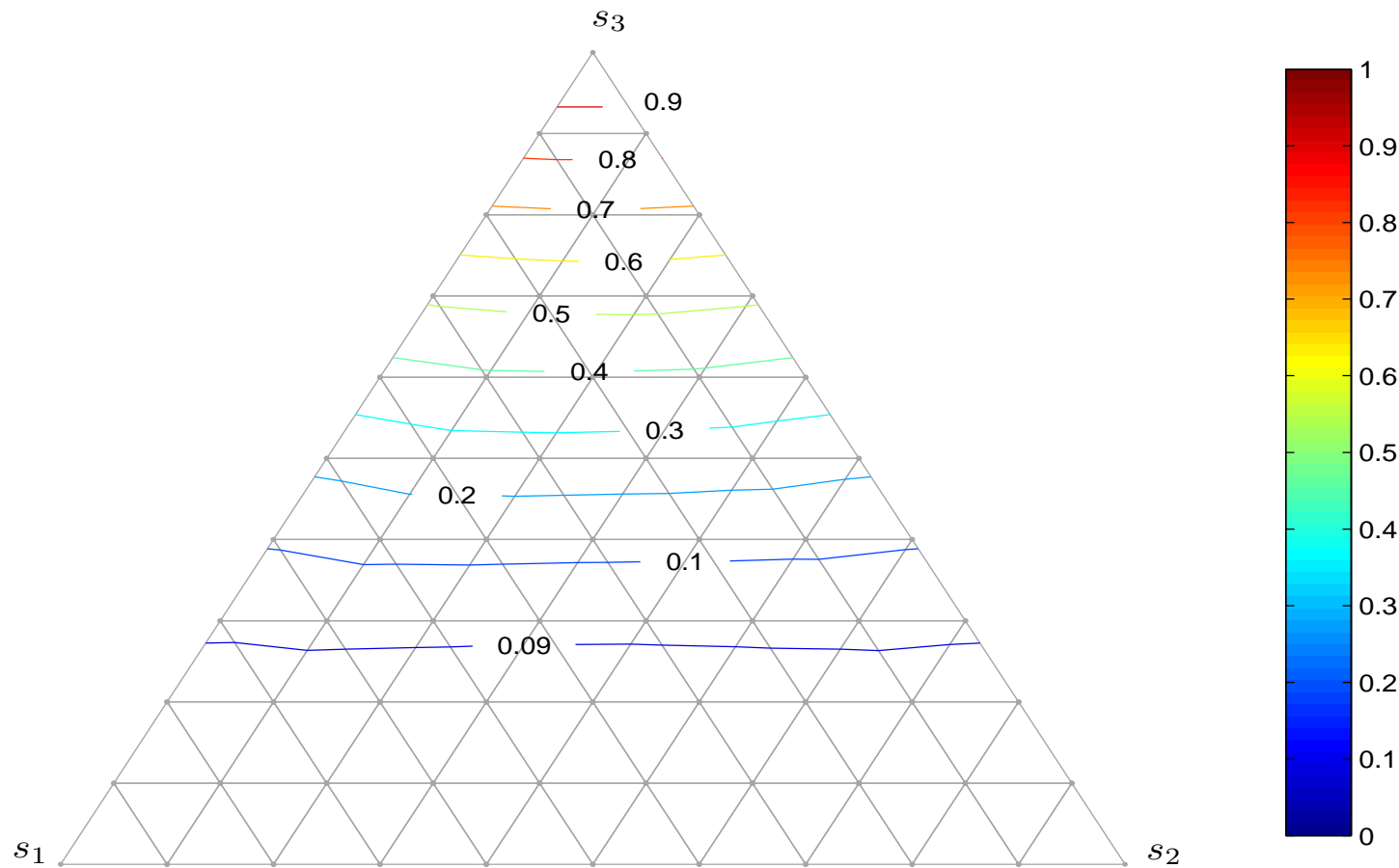
# INTERPOLATION - Back to relative permeabilities :

- **Step 2** :  $P_{cg}, d \Rightarrow$  TD Three-phase relative permeabilities



# INTERPOLATION - Back to relative permeabilities :

- **Step 2** :  $P_{cg}, d \Rightarrow$  TD Three-phase relative permeabilities



## Conclusion

For three-phase compressible flows :

- Equivalent **global pressure** formulation :  
**no gradient of capillary pressure in pressure equation !**
- Well defined transformation ( $0 \leq \partial P_{cg} / \partial p < 1$ )
- the **global pressure**  $p$  is a good numerical unknown !  
**remains smooth when the mobility of one fluid vanishes**

## Conclusion

For three-phase compressible flows :

- Equivalent **global pressure** formulation :  
**no gradient of capillary pressure in pressure equation !**
- Well defined transformation ( $0 \leq \partial P_{cg} / \partial p < 1$ )
- the **global pressure**  $p$  is a good numerical unknown !  
**remains smooth when the mobility of one fluid vanishes**

Bad news : three-phase data have to satisfy a **TD condition**

Good news : **TD relative permeabilities** can be **INTERPOLATED**  
from classical **water-oil**, **gas-oil** and **water-gas** two-phase data.

## Conclusion

For three-phase compressible flows :

- Equivalent **global pressure** formulation :  
**no gradient of capillary pressure in pressure equation !**
- Well defined transformation ( $0 \leq \partial P_{cg} / \partial p < 1$ )
- the **global pressure**  $p$  is a good numerical unknown !  
**remains smooth when the mobility of one fluid vanishes**

Bad news : three-phase data have to satisfy a **TD condition**

Good news : **TD relative permeabilities** can be **INTERPOLATED**  
from classical **water-oil**, **gas-oil** and **water-gas** two-phase data.

Next step : replace **INTERPOLATION** by **OPTIMIZATION** :

- take constraints into account,
- try to match  $kr_j^{\text{target}}(s), j = 1 \dots 3$ .